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Important Formulas in Mass Transfer Coefficient, Driving Force and Theories

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List of 29 Important Formulas in Mass Transfer Coefficient, Driving Force and Theories

Important Formulas in Mass Transfer Coefficient, Driving Force and Theories

1) Average Mass Transfer Coefficient by Penetration Theory

$$\text{fx } k_L (\text{Avg}) = 2 \cdot \sqrt{\frac{D_{AB}}{\pi \cdot t_c}}$$

[Open Calculator !\[\]\(a870788d6ed9b8fd294b7654a8c8526b_img.jpg\)](#)

$$\text{ex } 0.028465 \text{m/s} = 2 \cdot \sqrt{\frac{0.007 \text{m}^2/\text{s}}{\pi \cdot 11 \text{s}}}$$

2) Average Sherwood Number of Combined Laminar and Turbulent Flow

$$\text{fx } N_{sh} = ((0.037 \cdot (Re^{0.8})) - 871) \cdot (Sc^{0.333})$$

[Open Calculator !\[\]\(c50c8b7b2cc2cf9ff925edec0ee94c0d_img.jpg\)](#)

$$\text{ex } 1074.78 = ((0.037 \cdot ((500000)^{0.8})) - 871) \cdot ((12)^{0.333})$$

3) Average Sherwood Number of Flat Plate Turbulent Flow

$$\text{fx } N_{sh} = 0.037 \cdot (Re^{0.8})$$

[Open Calculator !\[\]\(f60b7a900783ac3fd531bfd9c111be6d_img.jpg\)](#)

$$\text{ex } 1340.842 = 0.037 \cdot ((500000)^{0.8})$$



4) Average Sherwood Number of Internal Turbulent Flow

$$\text{fx } N_{sh} = 0.023 \cdot (Re^{0.83}) \cdot (Sc^{0.44})$$

Open Calculator 

$$\text{ex } 3687.336 = 0.023 \cdot ((500000)^{0.83}) \cdot ((12)^{0.44})$$

5) Convective Mass Transfer Coefficient

$$\text{fx } k_L = \frac{m_a}{\rho_{a1} - \rho_{a2}}$$

Open Calculator 

$$\text{ex } 0.45 \text{m/s} = \frac{9 \text{kg/s/m}^2}{40 \text{kg/m}^3 - 20 \text{kg/m}^3}$$

6) Convective Mass Transfer Coefficient for Simultaneous Heat and Mass Transfer

$$\text{fx } k_L = \frac{h_t}{Q_s \cdot \rho_L \cdot (L_e^{0.67})}$$

Open Calculator 

$$\text{ex } 4 \times 10^{-5} \text{m/s} = \frac{13.2 \text{W/m}^2 \cdot \text{K}}{120 \text{J/(kg} \cdot \text{K)} \cdot 1000 \text{kg/m}^3 \cdot ((4.5)^{0.67})}$$



7) Convective Mass Transfer Coefficient of Flat Plate in Combined Laminar Turbulent Flow

$$\text{fx } k_L = \frac{0.0286 \cdot u_\infty}{(\text{Re}^{0.2}) \cdot (\text{Sc}^{0.67})}$$

Open Calculator 

$$\text{ex } 0.004118\text{m/s} = \frac{0.0286 \cdot 10.5\text{m/s}}{\left((500000)^{0.2}\right) \cdot \left((12)^{0.67}\right)}$$

8) Convective Mass Transfer Coefficient of Flat Plate Laminar Flow using Drag Coefficient

$$\text{fx } k_L = \frac{C_D \cdot u_\infty}{2 \cdot (\text{Sc}^{0.67})}$$

Open Calculator 

$$\text{ex } 29.80088\text{m/s} = \frac{30 \cdot 10.5\text{m/s}}{2 \cdot \left((12)^{0.67}\right)}$$

9) Convective Mass Transfer Coefficient of Flat Plate Laminar Flow using Friction Factor

$$\text{fx } k_L = \frac{f \cdot u_\infty}{8 \cdot (\text{Sc}^{0.67})}$$

Open Calculator 

$$\text{ex } 0.156455\text{m/s} = \frac{0.63 \cdot 10.5\text{m/s}}{8 \cdot \left((12)^{0.67}\right)}$$



10) Convective Mass Transfer Coefficient of Flat Plate Laminar Flow using Reynolds Number

$$\text{fx } k_L = \frac{u_\infty \cdot 0.322}{(\text{Re}^{0.5}) \cdot (\text{Sc}^{0.67})}$$

Open Calculator 

$$\text{ex } 0.000905 \text{m/s} = \frac{10.5 \text{m/s} \cdot 0.322}{((500000)^{0.5}) \cdot ((12)^{0.67})}$$

11) Convective Mass Transfer Coefficient through Liquid Gas Interface

$$\text{fx } k_L = \frac{m_1 \cdot m_2 \cdot H}{(m_1 \cdot H) + (m_2)}$$

Open Calculator 

$$\text{ex } 0.004767 \text{m/s} = \frac{0.3 \text{m/s} \cdot 0.7 \text{m/s} \cdot 0.016}{(0.3 \text{m/s} \cdot 0.016) + (0.7 \text{m/s})}$$

12) Fractional Resistance Offered by Gas Phase

$$\text{fx } \text{FR}_g = \frac{\frac{1}{k_y}}{\frac{1}{K_y}}$$

Open Calculator 

$$\text{ex } 0.84966 = \frac{\frac{1}{90 \text{mol/s}^* \text{m}^2}}{\frac{1}{76.46939 \text{mol/s}^* \text{m}^2}}$$



13) Fractional Resistance Offered by Liquid Phase

$$\text{fx } FR_l = \frac{\frac{1}{k_x}}{\frac{1}{K_x}}$$

[Open Calculator !\[\]\(d3fb9f94af8b26d1c844efa9a98805b0_img.jpg\)](#)

$$\text{ex } 0.183673 = \frac{\frac{1}{9.2\text{mol/s}^*\text{m}^2}}{\frac{1}{1.689796\text{mol/s}^*\text{m}^2}}$$

14) Gas Phase Mass Transfer Coefficient by Two Film Theory

$$\text{fx } K_y = \frac{1}{\left(\frac{1}{k_y}\right) + \left(\frac{H}{k_x}\right)}$$

[Open Calculator !\[\]\(e1d6102fe77919492c04879c8450f1f5_img.jpg\)](#)

$$\text{ex } 77.81955\text{mol/s}^*\text{m}^2 = \frac{1}{\left(\frac{1}{90\text{mol/s}^*\text{m}^2}\right) + \left(\frac{0.016}{9.2\text{mol/s}^*\text{m}^2}\right)}$$

15) Gas Phase Mass Transfer Coefficient using Fractional Resistance by Gas Phase

$$\text{fx } k_y = \frac{K_y}{FR_g}$$

[Open Calculator !\[\]\(ab4e2b3fc7e7887b7a72f548aa6f5e60_img.jpg\)](#)

$$\text{ex } 89.99999\text{mol/s}^*\text{m}^2 = \frac{76.46939\text{mol/s}^*\text{m}^2}{0.84966}$$



16) Heat Transfer Coefficient for Simultaneous Heat and Mass Transfer

$$\text{fx } h_t = k_L \cdot \rho_L \cdot Q_s \cdot (L_e^{0.67})$$

Open Calculator 

ex

$$1479.266 \text{ W/m}^2 \cdot \text{K} = 4.5 \text{e-}3 \text{ m/s} \cdot 1000 \text{ kg/m}^3 \cdot 120 \text{ J/(kg} \cdot \text{K)} \cdot ((4.5)^{0.67})$$

17) Liquid Phase Mass Transfer Coefficient by Two Film Theory

$$\text{fx } K_x = \frac{1}{\left(\frac{1}{k_y \cdot H}\right) + \left(\frac{1}{k_x}\right)}$$

Open Calculator 

ex

$$1.245113 \text{ mol/s} \cdot \text{m}^2 = \frac{1}{\left(\frac{1}{90 \text{ mol/s} \cdot \text{m}^2 \cdot 0.016}\right) + \left(\frac{1}{9.2 \text{ mol/s} \cdot \text{m}^2}\right)}$$

18) Liquid Phase Mass Transfer Coefficient using Fractional Resistance by Liquid Phase

$$\text{fx } k_x = \frac{K_x}{FR_l}$$

Open Calculator 

ex

$$9.200024 \text{ mol/s} \cdot \text{m}^2 = \frac{1.689796 \text{ mol/s} \cdot \text{m}^2}{0.183673}$$

19) Local Sherwood Number for Flat Plate in Laminar Flow

$$\text{fx } L_{sh} = 0.332 \cdot (Re_l^{0.5}) \cdot (Sc^{0.333})$$

Open Calculator 

ex

$$0.563231 = 0.332 \cdot ((0.55)^{0.5}) \cdot ((12)^{0.333})$$



20) Local Sherwood Number for Flat Plate in Turbulent Flow

$$\text{fx } L_{sh} = 0.0296 \cdot (Re_1^{0.8}) \cdot (Sc^{0.333})$$

[Open Calculator !\[\]\(6605b201d6f14d9b3bcb8ab5f274d107_img.jpg\)](#)

$$\text{ex } 0.041971 = 0.0296 \cdot ((0.55)^{0.8}) \cdot ((12)^{0.333})$$

21) Logarithmic Mean of Concentration Difference

$$\text{fx } C_{bm} = \frac{C_{b2} - C_{b1}}{\ln\left(\frac{C_{b2}}{C_{b1}}\right)}$$

[Open Calculator !\[\]\(e8fb589d58dad1692debababa5e928b6_img.jpg\)](#)

$$\text{ex } 12.33152 \text{mol/L} = \frac{10 \text{mol/L} - 15 \text{mol/L}}{\ln\left(\frac{10 \text{mol/L}}{15 \text{mol/L}}\right)}$$

22) Logarithmic Mean Partial Pressure Difference

$$\text{fx } P_{bm} = \frac{P_{b2} - P_{b1}}{\ln\left(\frac{P_{b2}}{P_{b1}}\right)}$$

[Open Calculator !\[\]\(4688aadfd656ded00cd6bdfae55089a9_img.jpg\)](#)

$$\text{ex } 9571.809 \text{Pa} = \frac{10500 \text{Pa} - 8700 \text{Pa}}{\ln\left(\frac{10500 \text{Pa}}{8700 \text{Pa}}\right)}$$

23) Mass Transfer Boundary Layer Thickness of Flat Plate in Laminar Flow

$$\text{fx } \delta_{mx} = \delta_{hx} \cdot (Sc^{-0.333})$$

[Open Calculator !\[\]\(4146d17f71dced09c6ad789cacceaa6d_img.jpg\)](#)

$$\text{ex } 3.715794 = 8.5 \text{m} \cdot ((12)^{-0.333})$$



24) Mass Transfer Coefficient by Film Theory

$$\text{fx } k_L = \frac{D_{AB}}{\delta}$$

Open Calculator 

$$\text{ex } 1.4\text{m/s} = \frac{0.007\text{m}^2/\text{s}}{0.005\text{m}}$$

25) Mass Transfer Coefficient by Surface Renewal Theory

$$\text{fx } k_L = \sqrt{D_{AB} \cdot s}$$

Open Calculator 

$$\text{ex } 0.009165\text{m/s} = \sqrt{0.007\text{m}^2/\text{s} \cdot 0.012/\text{s}}$$

26) Mass Transfer Stanton Number

$$\text{fx } St_m = \frac{k_L}{u_\infty}$$

Open Calculator 

$$\text{ex } 0.000429 = \frac{4.5\text{e-}3\text{m/s}}{10.5\text{m/s}}$$

27) Overall Gas Phase Mass Transfer Coefficient using Fractional Resistance by Gas Phase

$$\text{fx } K_y = k_y \cdot FR_g$$

Open Calculator 

$$\text{ex } 76.4694\text{mol/s}^*\text{m}^2 = 90\text{mol/s}^*\text{m}^2 \cdot 0.84966$$



28) Overall Liquid Phase Mass Transfer Coefficient using Fractional Resistance by Liquid Phase

$$\text{fx } K_x = k_x \cdot FR_l$$

[Open Calculator !\[\]\(8b57f0e15e7dda24cf9977561475f640_img.jpg\)](#)

$$\text{ex } 1.689792 \text{mol/s}^* \text{m}^2 = 9.2 \text{mol/s}^* \text{m}^2 \cdot 0.183673$$

29) Sherwood Number for Flat Plate in Laminar Flow

$$\text{fx } N_{sh} = 0.664 \cdot (Re^{0.5}) \cdot (Sc^{0.333})$$

[Open Calculator !\[\]\(ceb7cef9f9d693d102dfe501130037c6_img.jpg\)](#)

$$\text{ex } 1074.04 = 0.664 \cdot ((500000)^{0.5}) \cdot ((12)^{0.333})$$



Variables Used

- C_{b1} Concentration of Component B in Mixture 1 (Mole per Liter)
- C_{b2} Concentration of Component B in Mixture 2 (Mole per Liter)
- C_{bm} Logarithmic Mean of Concentration Difference (Mole per Liter)
- C_D Drag Coefficient
- D_{AB} Diffusion Coefficient (DAB) (Square Meter Per Second)
- f Friction Factor
- FR_g Fractional Resistance Offered by Gas Phase
- FR_l Fractional Resistance Offered by Liquid Phase
- H Henry's Constant
- h_t Heat Transfer Coefficient (Watt per Square Meter per Kelvin)
- k_L (Avg) Average Convective Mass Transfer Coefficient (Meter per Second)
- k_L Convective Mass Transfer Coefficient (Meter per Second)
- k_L Convective Mass Transfer Coefficient (Meter per Second)
- k_x Liquid Phase Mass Transfer Coefficient (Mole per Second Square Meter)
- K_x Overall Liquid Phase Mass Transfer Coefficient (Mole per Second Square Meter)
- k_y Gas Phase Mass Transfer Coefficient (Mole per Second Square Meter)
- K_y Overall Gas Phase Mass Transfer Coefficient (Mole per Second Square Meter)
- L_e Lewis Number










- L_{sh} Local Sherwood Number
- m_1 Mass Transfer Coefficient of Medium 1 (Meter per Second)
- m_2 Mass Transfer Coefficient of Medium 2 (Meter per Second)
- m_a Mass Flux of Diffusion Component A (Kilogram per Second per Square Meter)
- N_{sh} Average Sherwood Number
- P_{b1} Partial Pressure of Component B in 1 (Pascal)
- P_{b2} Partial Pressure of Component B in 2 (Pascal)
- P_{bm} Logarithmic Mean Partial Pressure Difference (Pascal)
- Q_s Specific Heat (Joule per Kilogram per K)
- Re Reynolds Number
- Re_l Local Reynolds Number
- s Surface Renewal Rate (1 Per Second)
- Sc Schmidt Number
- St_m Mass Transfer Stanton Number
- t_c Average Contact Time (Second)
- u_∞ Free Stream Velocity (Meter per Second)
- δ Film Thickness (Meter)
- δ_{mx} Mass Transfer Boundary Layer Thickness at x
- ρ_{a1} Mass Concentration of Component A in Mixture 1 (Kilogram per Cubic Meter)
- ρ_{a2} Mass Concentration of Component A in Mixture 2 (Kilogram per Cubic Meter)
- ρ_L Density of Liquid (Kilogram per Cubic Meter)



- δ_{hx} Hydrodynamic Boundary Layer Thickness (Meter)



Constants, Functions, Measurements used

- **Constant:** **pi**, 3.14159265358979323846264338327950288
Archimedes' constant
- **Function:** **ln**, $\ln(\text{Number})$
The natural logarithm, also known as the logarithm to the base e, is the inverse function of the natural exponential function.
- **Function:** **sqrt**, $\text{sqrt}(\text{Number})$
A square root function is a function that takes a non-negative number as an input and returns the square root of the given input number.
- **Measurement:** **Length** in Meter (m)
Length Unit Conversion 
- **Measurement:** **Time** in Second (s)
Time Unit Conversion 
- **Measurement:** **Pressure** in Pascal (Pa)
Pressure Unit Conversion 
- **Measurement:** **Speed** in Meter per Second (m/s)
Speed Unit Conversion 
- **Measurement:** **Specific Heat Capacity** in Joule per Kilogram per K ($\text{J}/(\text{kg}\cdot\text{K})$)
Specific Heat Capacity Unit Conversion 
- **Measurement:** **Heat Transfer Coefficient** in Watt per Square Meter per Kelvin ($\text{W}/\text{m}^2\cdot\text{K}$)
Heat Transfer Coefficient Unit Conversion 
- **Measurement:** **Molar Concentration** in Mole per Liter (mol/L)
Molar Concentration Unit Conversion 
- **Measurement:** **Mass Flux** in Kilogram per Second per Square Meter ($\text{kg}/\text{s}/\text{m}^2$)



Mass Flux Unit Conversion 

- **Measurement: Density** in Kilogram per Cubic Meter (kg/m^3)

Density Unit Conversion 

- **Measurement: Diffusivity** in Square Meter Per Second (m^2/s)

Diffusivity Unit Conversion 

- **Measurement: Molar Flux of Diffusing Component** in Mole per Second Square Meter ($\text{mol/s}\cdot\text{m}^2$)

Molar Flux of Diffusing Component Unit Conversion 

- **Measurement: Time Inverse** in 1 Per Second ($1/\text{s}$)

Time Inverse Unit Conversion 



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