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Boiling Formulas

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List of 14 Boiling Formulas

Boiling ↗

1) Correlation for Heat Flux proposed by Mostinski ↗

fx $h_b = 0.00341 \cdot (P_c^{2.3}) \cdot (T_e^{2.33}) \cdot (P_r^{0.566})$

[Open Calculator ↗](#)

ex $110240.4 \text{ W/m}^2 \cdot {}^\circ\text{C} = 0.00341 \cdot ((5.9 \text{ Pa})^{2.3}) \cdot ((10 {}^\circ\text{C})^{2.33}) \cdot ((1.1)^{0.566})$

2) Critical Heat Flux by Zuber ↗

fx $q_{\text{Max}} = \left((0.149 \cdot L_v \cdot \rho_v) \cdot \left(\frac{(\sigma \cdot [g]) \cdot (\rho_L - \rho_v)}{\rho_v^2} \right)^{\frac{1}{4}} \right)$

[Open Calculator ↗](#)

ex

$58.17133 \text{ W/m}^2 = \left((0.149 \cdot 19 \text{ J/mol} \cdot 0.5 \text{ kg/m}^3) \cdot \left(\frac{(72.75 \text{ N/m} \cdot [g]) \cdot (1000 \text{ kg/m}^3 - 0.5 \text{ kg/m}^3)}{(0.5 \text{ kg/m}^3)^2} \right)^{\frac{1}{4}} \right)$

3) Excess Temperature in Boiling ↗

fx $T_{\text{excess}} = T_{\text{surface}} - T_{\text{Sat}}$

[Open Calculator ↗](#)

ex $297 \text{ K} = 670 \text{ K} - 373 \text{ K}$

4) Heat Flux in Fully Developed Boiling State for Higher Pressures ↗

fx $q_{\text{rate}} = 283.2 \cdot A \cdot ((\Delta T_x)^3) \cdot ((p_{\text{HT}})^{\frac{4}{3}})$

[Open Calculator ↗](#)

ex $150.3508 \text{ W} = 283.2 \cdot 5 \text{ m}^2 \cdot ((2.25 {}^\circ\text{C})^3) \cdot ((3 \times 10^{-8} \text{ MPa})^{\frac{4}{3}})$

5) Heat Flux in Fully Developed Boiling State for Pressure upto 0.7 Megapascal ↗

fx $q_{\text{rate}} = 2.253 \cdot A \cdot ((\Delta T_x)^{3.96})$

[Open Calculator ↗](#)

ex $279.495 \text{ W} = 2.253 \cdot 5 \text{ m}^2 \cdot ((2.25 {}^\circ\text{C})^{3.96})$



6) Heat Transfer Coefficient for Forced Convection Local Boiling Inside Vertical Tubes ↗

$$fx \quad h = \left(2.54 \cdot \left((\Delta T_x)^3 \right) \cdot \exp\left(\frac{p}{1.551}\right) \right)$$

[Open Calculator ↗](#)

$$ex \quad 29.04564 \text{W/m}^2\text{*}^\circ\text{C} = \left(2.54 \cdot \left((2.25 \text{ }^\circ\text{C})^3 \right) \cdot \exp\left(\frac{0.00607 \text{MPa}}{1.551}\right) \right)$$

7) Heat Transfer Coefficient given Biot Number ↗

$$fx \quad h_{\text{transfer}} = \frac{Bi \cdot k}{\ell}$$

[Open Calculator ↗](#)

$$ex \quad 4.467776 \text{W/m}^2\text{*K} = \frac{2.19 \cdot 10.18 \text{W/(m*K)}}{4.99 \text{m}}$$

8) Modified Heat of Vaporization ↗

$$fx \quad \lambda = \left(h_{fg} + (c_{pv}) \cdot \left(\frac{T_w - T_{\text{Sat}}}{2} \right) \right)$$

[Open Calculator ↗](#)

$$ex \quad 2636 \text{J/kg} = \left(2260 \text{J/kg} + (23.5 \text{J/(kg*K)}) \cdot \left(\frac{405 \text{K} - 373 \text{K}}{2} \right) \right)$$

9) Modified Heat Transfer Coefficient under Influence of Pressure ↗

$$fx \quad h_p = (h_1) \cdot \left(\left(\frac{p_s}{p_1} \right)^{0.4} \right)$$

[Open Calculator ↗](#)

$$ex \quad 44.95387 \text{W/m}^2\text{*K} = (10.9 \text{W/m}^2\text{*K}) \cdot \left(\left(\frac{3.5 \text{Pa}}{0.101325 \text{Pa}} \right)^{0.4} \right)$$

10) Radiation Heat Transfer Coefficient ↗

$$fx \quad h_r = \left(\frac{[\text{Stefan-BoltZ}] \cdot \varepsilon \cdot \left((T_w)^4 - (T_{\text{Sat}})^4 \right)}{T_w - T_{\text{Sat}}} \right)$$

[Open Calculator ↗](#)

$$ex \quad 12.70509 \text{W/m}^2\text{*K} = \left(\frac{[\text{Stefan-BoltZ}] \cdot 0.95 \cdot \left((405 \text{K})^4 - (373 \text{K})^4 \right)}{405 \text{K} - 373 \text{K}} \right)$$



11) Radius of Vapour Bubble in Mechanical Equilibrium in Superheated Liquid ↗

[Open Calculator ↗](#)

$$fx \quad r = \frac{2 \cdot \sigma \cdot [R] \cdot (T_{\text{Sat}}^2)}{P_1 \cdot L_v \cdot (T_1 - T_{\text{Sat}})}$$

$$ex \quad 0.14151m = \frac{2 \cdot 72.75N/m \cdot [R] \cdot ((373K)^2)}{200000Pa \cdot 19J/mol \cdot (686K - 373K)}$$

12) Saturated Temperature given Excess Temperature ↗

[Open Calculator ↗](#)

$$fx \quad T_{\text{Sat}} = T_{\text{surface}} - T_{\text{excess}}$$

$$ex \quad 373K = 670K - 297K$$

13) Surface Temperature given Excess Temperature ↗

[Open Calculator ↗](#)

$$fx \quad T_{\text{surface}} = T_{\text{Sat}} + T_{\text{excess}}$$

$$ex \quad 670K = 373K + 297K$$

14) Total Heat Transfer Coefficient ↗

[Open Calculator ↗](#)

$$fx \quad h_T = h_{FB} \cdot \left(\left(\frac{h_{FB}}{h_{\text{transfer}}} \right)^{\frac{1}{3}} \right) + h_r$$

$$ex \quad 5449.994W/m^2*K = 921W/m^2*K \cdot \left(\left(\frac{921W/m^2*K}{4.476W/m^2*K} \right)^{\frac{1}{3}} \right) + 12.70W/m^2*K$$



Variables Used

- A Area (Square Meter)
- Bi Biot Number
- C_{pv} Specific Heat of Water Vapor (Joule per Kilogram per K)
- h Heat Transfer Coefficient for Forced Convection (Watt per Square Meter per Celcius)
- h_1 Heat Transfer Coefficient at Atmospheric Pressure (Watt per Square Meter per Kelvin)
- h_b Heat Transfer Coefficient For Nucleate Boiling (Watt per Square Meter per Celcius)
- h_{FB} Heat Transfer Coefficient in Film Boiling Region (Watt per Square Meter per Kelvin)
- h_{fg} Latent Heat of Vaporization (Joule per Kilogram)
- h_p Heat Transfer Coefficient at Some Pressure P (Watt per Square Meter per Kelvin)
- h_r Radiation Heat Transfer Coefficient (Watt per Square Meter per Kelvin)
- h_T Total Heat Transfer Coefficient (Watt per Square Meter per Kelvin)
- $h_{transfer}$ Heat Transfer Coefficient (Watt per Square Meter per Kelvin)
- k Thermal Conductivity (Watt per Meter per K)
- L_v Enthalpy of Vaporization of Liquid (Joule Per Mole)
- p System Pressure in Vertical Tubes (Megapascal)
- p_1 Standard Atmospheric Pressure (Pascal)
- P_c Critical Pressure (Pascal)
- P_{HT} Pressure (Megapascal)
- P_l Pressure of Superheated Liquid (Pascal)
- P_r Reduced Pressure
- p_s System Pressure (Pascal)
- q_{Max} Critical Heat Flux (Watt per Square Meter)
- q_{rate} Rate of Heat Transfer (Watt)
- r Radius of Vapor Bubble (Meter)
- T_e Excess Temperature in Nucleate Boiling (Celsius)
- T_{excess} Excess Temperature in Heat Transfer (Kelvin)
- T_l Temperature of Superheated Liquid (Kelvin)
- T_{Sat} Saturation Temperature (Kelvin)
- $T_{surface}$ Surface Temperature (Kelvin)
- T_w Plate Surface Temperature (Kelvin)
- ΔT_x Excess Temperature (Degree Celsius)



- ϵ Emissivity
- λ Modified Heat of Vaporization (Joule per Kilogram)
- ρ_L Density of Liquid (Kilogram per Cubic Meter)
- ρ_v Density of Vapor (Kilogram per Cubic Meter)
- σ Surface Tension (Newton per Meter)
- ℓ Thickness of Wall (Meter)



Constants, Functions, Measurements used

- **Constant:** [g], 9.80665 Meter/Second²
Gravitational acceleration on Earth
- **Constant:** [Stefan-BoltZ], 5.670367E-8 Kilogram Second⁻³ Kelvin⁻⁴
Stefan-Boltzmann Constant
- **Constant:** [R], 8.31446261815324 Joule / Kelvin * Mole
Universal gas constant
- **Function:** exp, exp(Number)
Exponential function
- **Measurement:** Length in Meter (m)
Length Unit Conversion ↗
- **Measurement:** Temperature in Celsius (°C), Kelvin (K)
Temperature Unit Conversion ↗
- **Measurement:** Area in Square Meter (m²)
Area Unit Conversion ↗
- **Measurement:** Pressure in Pascal (Pa), Megapascal (MPa)
Pressure Unit Conversion ↗
- **Measurement:** Temperature Difference in Degree Celsius (°C)
Temperature Difference Unit Conversion ↗
- **Measurement:** Thermal Conductivity in Watt per Meter per K (W/(m*K))
Thermal Conductivity Unit Conversion ↗
- **Measurement:** Specific Heat Capacity in Joule per Kilogram per K (J/(kg*K))
Specific Heat Capacity Unit Conversion ↗
- **Measurement:** Heat Flux Density in Watt per Square Meter (W/m²)
Heat Flux Density Unit Conversion ↗
- **Measurement:** Heat Transfer Coefficient in Watt per Square Meter per Celcius (W/m²*°C), Watt per Square Meter per Kelvin (W/m²*K)
Heat Transfer Coefficient Unit Conversion ↗
- **Measurement:** Surface Tension in Newton per Meter (N/m)
Surface Tension Unit Conversion ↗
- **Measurement:** Density in Kilogram per Cubic Meter (kg/m³)
Density Unit Conversion ↗
- **Measurement:** Latent Heat in Joule per Kilogram (J/kg)
Latent Heat Unit Conversion ↗
- **Measurement:** Energy Per Mole in Joule Per Mole (J/mol)
Energy Per Mole Unit Conversion ↗
- **Measurement:** Rate of Heat Transfer in Watt (W)
Rate of Heat Transfer Unit Conversion ↗



Check other formula lists

- Boiling Formulas 
- Condensation Formulas 
- Important Formulas of Condensation Number, Average Heat Transfer Coefficient and Heat Flux 

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