## Important Formulas in Potpourri of Multiple Reactions

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## List of 26 Important Formulas in Potpourri of Multiple Reactions

## Important Formulas in Potpourri of Multiple Reactions

1) Initial Reactant Concentration for First Order Rxn for MFR using Intermediate Concentration
$f \times \mathrm{C}_{\mathrm{A} 0}=\frac{\mathrm{C}_{\mathrm{R}} \cdot\left(1+\left(\mathrm{k}_{\mathrm{I}} \cdot \tau_{\mathrm{m}}\right)\right) \cdot\left(1+\left(\mathrm{k}_{2} \cdot \tau_{\mathrm{m}}\right)\right)}{\mathrm{k}_{\mathrm{I}} \cdot \tau_{\mathrm{m}}}$
ex $23.48889 \mathrm{~mol} / \mathrm{m}^{3}=\frac{10 \mathrm{~mol} / \mathrm{m}^{3} \cdot\left(1+\left(0.42 \mathrm{~s}^{-1} \cdot 12 \mathrm{~s}\right)\right) \cdot\left(1+\left(0.08 \mathrm{~s}^{-1} \cdot 12 \mathrm{~s}\right)\right)}{0.42 \mathrm{~s}^{-1} \cdot 12 \mathrm{~s}}$
2) Initial Reactant Concentration for First Order Rxn in MFR at Maximum Intermediate Concentration
$f \mathrm{fx} \mathrm{C}_{\mathrm{A} 0}=\mathrm{C}_{\mathrm{R}, \max } \cdot\left(\left(\left(\left(\frac{\mathrm{k}_{2}}{\mathrm{k}_{\mathrm{I}}}\right)^{\frac{1}{2}}\right)+1\right)^{2}\right)$
ex $82.53391 \mathrm{~mol} / \mathrm{m}^{3}=40 \mathrm{~mol} / \mathrm{m}^{3} \cdot\left(\left(\left(\left(\frac{0.08 \mathrm{~s}^{-1}}{0.42 \mathrm{~s}^{-1}}\right)^{\frac{1}{2}}\right)+1\right)^{2}\right)$
3) Initial Reactant Concentration for First Order Rxn in Series for Maximum Intermediate Concentration
$f \times \mathrm{C}_{\mathrm{A} 0}=\frac{\mathrm{C}_{\mathrm{R}, \max }}{\left(\frac{\mathrm{k}_{\mathrm{I}}}{\mathrm{k}_{2}}\right)^{\frac{k_{2}}{k_{2}-k_{1}}}}$
ex $59.08935 \mathrm{~mol} / \mathrm{m}^{3}=\frac{40 \mathrm{~mol} / \mathrm{m}^{3}}{\left(\frac{0.42 \mathrm{~s}^{-1}}{0.08 \mathrm{~s}^{-1}}\right)^{\frac{0.08 s^{-1}}{0.08 s^{1}-0.42 s^{-1}}}}$

4）Initial Reactant Concentration for First Order Rxn in Series for MFR using Product Concentration む
$f \mathrm{C} \mathrm{C}_{\mathrm{A} 0}=\frac{\mathrm{C}_{\mathrm{S}} \cdot\left(1+\left(\mathrm{k}_{\mathrm{I}} \cdot \tau_{\mathrm{m}}\right)\right) \cdot\left(1+\left(\mathrm{k}_{2} \cdot \tau_{\mathrm{m}}\right)\right)}{\mathrm{k}_{\mathrm{I}} \cdot \mathrm{k}_{2} \cdot\left(\tau_{\mathrm{m}}^{2}\right)}$
ex $48.93519 \mathrm{~mol} / \mathrm{m}^{3}=\frac{20 \mathrm{~mol} / \mathrm{m}^{3} \cdot\left(1+\left(0.42 \mathrm{~s}^{-1} \cdot 12 \mathrm{~s}\right)\right) \cdot\left(1+\left(0.08 \mathrm{~s}^{-1} \cdot 12 \mathrm{~s}\right)\right)}{0.42 \mathrm{~s}^{-1} \cdot 0.08 \mathrm{~s}^{-1} \cdot\left((12 \mathrm{~s})^{2}\right)}$
5）Initial Reactant Concentration for Two Steps First Order Irreversible Reaction in Series
$f \mathrm{fx} \mathrm{C}_{\mathrm{A} 0}=\frac{\mathrm{C}_{\mathrm{R}} \cdot\left(\mathrm{k}_{2}-\mathrm{k}_{\mathrm{I}}\right)}{\mathrm{k}_{\mathrm{I}} \cdot\left(\exp \left(-\mathrm{k}_{\mathrm{I}} \cdot \tau\right)-\exp \left(-\mathrm{k}_{2} \cdot \tau\right)\right)}$
Open Calculator
ex $89.23855 \mathrm{~mol} / \mathrm{m}^{3}=\frac{10 \mathrm{~mol} / \mathrm{m}^{3} \cdot\left(0.08 \mathrm{~s}^{-1}-0.42 \mathrm{~s}^{-1}\right)}{0.42 \mathrm{~s}^{-1} \cdot\left(\exp \left(-0.42 \mathrm{~s}^{-1} \cdot 30 \mathrm{~s}\right)-\exp \left(-0.08 \mathrm{~s}^{-1} \cdot 30 \mathrm{~s}\right)\right)}$
6）Initial Reactant Concentration for Two Steps First Order Reaction for Mixed Flow Reactor
$f \times \mathrm{C}_{\mathrm{A} 0}=\mathrm{C}_{\mathrm{k} 1} \cdot\left(1+\left(\mathrm{k}_{\mathrm{I}} \cdot \tau_{\mathrm{m}}\right)\right)$
Open Calculator
ex $80.332 \mathrm{~mol} / \mathrm{m}^{3}=13.3 \mathrm{~mol} / \mathrm{m}^{3} \cdot\left(1+\left(0.42 \mathrm{~s}^{-1} \cdot 12 \mathrm{~s}\right)\right)$
7）Initial Reactant Concentration in First Order followed by Zero Order Reaction
$f \times \mathrm{C}_{\mathrm{A} 0}=\frac{\mathrm{C}_{\mathrm{k} 0}}{\exp \left(-\mathrm{k}_{\mathrm{I}} \cdot \Delta \mathrm{t}\right)}$
Open Calculator
ex $84.61012 \mathrm{~mol} / \mathrm{m}^{3}=\frac{24 \mathrm{~mol} / \mathrm{m}^{3}}{\exp \left(-0.42 \mathrm{~s}^{-1} \cdot 3 \mathrm{~s}\right)}$

8）Initial Reactant Concentration using Intermediate for First Order followed by Zero Order Reaction区
$f \mathrm{f} \mathrm{C}_{\mathrm{A} 0 \text { for } \mathrm{R}}=\frac{\mathrm{C}_{\mathrm{R}}+\left(\mathrm{k}_{0} \cdot \Delta \mathrm{t}\right)}{1-\exp \left(-\mathrm{k}_{\mathrm{I}} \cdot \Delta \mathrm{t}\right)}$
ex $41.18122 \mathrm{~mol} / \mathrm{m}^{3}=\frac{10 \mathrm{~mol} / \mathrm{m}^{3}+\left(6.5 \mathrm{~mol} / \mathrm{m}^{3}{ }^{\mathrm{s}} \cdot 3 \mathrm{~s}\right)}{1-\exp \left(-0.42 \mathrm{~s}^{-1} \cdot 3 \mathrm{~s}\right)}$
9) Intermediate Concentration for First Order followed by Zero Order Reaction
$f \mathrm{f}$ C $\mathrm{C}_{\mathrm{R}, 1 \text { st order }}=\mathrm{C}_{\mathrm{A} 0} \cdot\left(1-\exp \left(-\mathrm{k}_{\mathrm{I}} \cdot \Delta \mathrm{t}\right)-\left(\frac{\mathrm{k}_{0} \cdot \Delta \mathrm{t}}{\mathrm{C}_{\mathrm{A} 0}}\right)\right)$
Open Calculator
ex $37.80768 \mathrm{~mol} / \mathrm{m}^{3}=80 \mathrm{~mol} / \mathrm{m}^{3} \cdot\left(1-\exp \left(-0.42 \mathrm{~s}^{-1} \cdot 3 \mathrm{~s}\right)-\left(\frac{6.5 \mathrm{~mol} / \mathrm{m}^{3} \mathrm{~s} \cdot 3 \mathrm{~s}}{80 \mathrm{~mol} / \mathrm{m}^{3}}\right)\right)$
10) Intermediate Concentration for First Order Reaction for Mixed Flow Reactor
$\mathrm{fx} \mathrm{C}_{\mathrm{R}}=\frac{\mathrm{C}_{\mathrm{A} 0} \cdot \mathrm{k}_{\mathrm{I}} \cdot \tau_{\mathrm{m}}}{\left(1+\left(\mathrm{k}_{\mathrm{I}} \cdot \tau_{\mathrm{m}}\right)\right) \cdot\left(1+\left(\mathrm{k}_{2} \cdot \tau_{\mathrm{m}}\right)\right)}$
Open Calculator
ex $34.05866 \mathrm{~mol} / \mathrm{m}^{3}=\frac{80 \mathrm{~mol} / \mathrm{m}^{3} \cdot 0.42 \mathrm{~s}^{-1} \cdot 12 \mathrm{~s}}{\left(1+\left(0.42 \mathrm{~s}^{-1} \cdot 12 \mathrm{~s}\right)\right) \cdot\left(1+\left(0.08 \mathrm{~s}^{-1} \cdot 12 \mathrm{~s}\right)\right)}$
11) Intermediate Concentration for Two Steps First Order Irreversible Reaction in Series
$f \mathrm{x} \mathrm{C}_{\mathrm{R}}=\mathrm{C}_{\mathrm{A} 0} \cdot\left(\frac{\mathrm{k}_{\mathrm{I}}}{\mathrm{k}_{2}-\mathrm{k}_{\mathrm{I}}}\right) \cdot\left(\exp \left(-\mathrm{k}_{\mathrm{I}} \cdot \tau\right)-\exp \left(-\mathrm{k}_{2} \cdot \tau\right)\right)$
Open Calculator
ex
$8.964735 \mathrm{~mol} / \mathrm{m}^{3}=80 \mathrm{~mol} / \mathrm{m}^{3} \cdot\left(\frac{0.42 \mathrm{~s}^{-1}}{0.08 \mathrm{~s}^{-1}-0.42 \mathrm{~s}^{-1}}\right) \cdot\left(\exp \left(-0.42 \mathrm{~s}^{-1} \cdot 30 \mathrm{~s}\right)-\exp \left(-0.08 \mathrm{~s}^{-1} \cdot 30 \mathrm{~s}\right)\right)$
12) Maximum Intermediate Concentration for First Order Irreversible Reaction in MFR
$f \times \mathrm{C}_{\mathrm{R}, \max }=\frac{\mathrm{C}_{\mathrm{A} 0}}{\left(\left(\left(\frac{\mathrm{k}_{2}}{\mathrm{k}_{\mathrm{I}}}\right)^{\frac{1}{2}}\right)+1\right)^{2}}$
ex $38.77194 \mathrm{~mol} / \mathrm{m}^{3}=\frac{80 \mathrm{~mol} / \mathrm{m}^{3}}{\left(\left(\left(\frac{0.08 \mathrm{~s}^{-1}}{0.42 \mathrm{~s}^{-1}}\right)^{\frac{1}{2}}\right)+1\right)^{2}}$
13) Maximum Intermediate Concentration for First Order Irreversible Reaction in Series
$f \mathrm{fx} \mathrm{C}_{\mathrm{R}, \max }=\mathrm{C}_{\mathrm{A} 0} \cdot\left(\frac{\mathrm{k}_{\mathrm{I}}}{\mathrm{k}_{2}}\right)^{\frac{\mathrm{k}_{2}}{\mathrm{k}_{2}-\mathrm{k}_{\mathrm{I}}}}$
ex $54.15527 \mathrm{~mol} / \mathrm{m}^{3}=80 \mathrm{~mol} / \mathrm{m}^{3} \cdot\left(\frac{0.42 \mathrm{~s}^{-1}}{0.08 \mathrm{~s}^{-1}}\right)^{\frac{0.08 \mathrm{~s}}{0.08 \mathrm{~s} \mathrm{~S}^{10.425}}}$
14) Maximum Intermediate Concentration in First Order followed by Zero Order Reaction
$f \mathrm{fx} \mathrm{C}_{\mathrm{R}, \max }=\mathrm{C}_{\mathrm{A} 0} \cdot\left(1-\left(\frac{\mathrm{k}_{0}}{\mathrm{C}_{\mathrm{A} 0} \cdot \mathrm{k}_{\mathrm{I}}} \cdot\left(1-\ln \left(\frac{\mathrm{k}_{0}}{\mathrm{C}_{\mathrm{A} 0} \cdot \mathrm{k}_{\mathrm{I}}}\right)\right)\right)\right)$
ex
$39.1007 \mathrm{~mol} / \mathrm{m}^{3}=80 \mathrm{~mol} / \mathrm{m}^{3} \cdot\left(1-\left(\frac{6.5 \mathrm{~mol} / \mathrm{m}^{3 *} \mathrm{~s}}{80 \mathrm{~mol} / \mathrm{m}^{3} \cdot 0.42 \mathrm{~s}^{-1}} \cdot\left(1-\ln \left(\frac{6.5 \mathrm{~mol} / \mathrm{m}^{3} \mathrm{~s}}{80 \mathrm{~mol} / \mathrm{m}^{3} \cdot 0.42 \mathrm{~s}^{-1}}\right)\right)\right)\right)$
15) Product Concentration for First Order Reaction for Mixed Flow Reactor
$\mathrm{fx} \mathrm{C}_{\mathrm{S}}=\frac{}{\left(1+\left(\mathrm{k}_{\mathrm{I}} \cdot \tau_{\mathrm{m}}\right)\right) \cdot\left(1+\left(\mathrm{k}_{2} \cdot \tau_{\mathrm{m}}\right)\right)}$
$32.69631 \mathrm{~mol} / \mathrm{m}^{3}=\frac{80 \mathrm{~mol} / \mathrm{m}^{3} \cdot 0.42 \mathrm{~s}^{-1} \cdot 0.08 \mathrm{~s}^{-1} \cdot\left((12 \mathrm{~s})^{2}\right)}{\left(1+\left(0.42 \mathrm{~s}^{-1} \cdot 12 \mathrm{~s}\right)\right) \cdot\left(1+\left(0.08 \mathrm{~s}^{-1} \cdot 12 \mathrm{~s}\right)\right)}$
16) Rate Constant for First Order Reaction in First Order followed by Zero Order Reaction
$f \mathrm{x} \mathrm{k}_{\mathrm{I}}=\left(\frac{1}{\Delta \mathrm{t}}\right) \cdot \ln \left(\frac{\mathrm{C}_{\mathrm{A} 0}}{\mathrm{C}_{\mathrm{k} 0}}\right)$
ex $0.401324 \mathrm{~s}^{-1}=\left(\frac{1}{3 \mathrm{~s}}\right) \cdot \ln \left(\frac{80 \mathrm{~mol} / \mathrm{m}^{3}}{24 \mathrm{~mol} / \mathrm{m}^{3}}\right)$
17) Rate Constant for First Order Reaction using Rate Constant for Zero Order Reaction
$f x \mathrm{k}_{\mathrm{I}}=\left(\frac{1}{\Delta \mathrm{t}}\right) \cdot \ln \left(\frac{\mathrm{C}_{\mathrm{A} 0}}{\mathrm{C}_{\mathrm{A} 0}-\left(\mathrm{k}_{0} \cdot \Delta \mathrm{t}\right)-\mathrm{C}_{\mathrm{R}}}\right)$
Open Calculator
ex $0.153351 \mathrm{~s}^{-1}=\left(\frac{1}{3 \mathrm{~s}}\right) \cdot \ln \left(\frac{80 \mathrm{~mol} / \mathrm{m}^{3}}{80 \mathrm{~mol} / \mathrm{m}^{3}-\left(6.5 \mathrm{~mol} / \mathrm{m}^{3} \mathrm{~s} \cdot 3 \mathrm{~s}\right)-10 \mathrm{~mol} / \mathrm{m}^{3}}\right)$
18) Rate Constant for First Step First Order Reaction for MFR at Maximum Intermediate Concentration $\qquad$
$\mathrm{fx}_{\mathrm{k}}^{\mathrm{k}}=\frac{1}{\mathrm{k}_{2} \cdot\left(\tau_{\mathrm{R}, \max }^{2}\right)}$
Open Calculator
ex $0.278458 \mathrm{~s}^{-1}=\frac{1}{0.08 \mathrm{~s}^{-1} \cdot\left((6.7 \mathrm{~s})^{2}\right)}$
19) Rate Constant for Second Step First Order Reaction for MFR at Maximum Intermediate Concentration
$\mathrm{fx} \mathrm{k}_{2}=\frac{1}{\mathrm{k}_{\mathrm{I}} \cdot\left(\tau_{\mathrm{R}, \max }^{2}\right)}$
ex $0.05304 \mathrm{~s}^{-1}=\frac{1}{0.42 \mathrm{~s}^{-1} \cdot\left((6.7 \mathrm{~s})^{2}\right)}$
20) Rate Constant for Zero Order Reaction using Rate Constant for First Order Reaction
$f \mathrm{x} \mathrm{k}_{0, \mathrm{k} 1}=\left(\frac{\mathrm{C}_{\mathrm{A} 0}}{\Delta \mathrm{t}}\right) \cdot\left(1-\exp \left(\left(-\mathrm{k}_{\mathrm{I}}\right) \cdot \Delta \mathrm{t}\right)-\left(\frac{\mathrm{C}_{\mathrm{R}}}{\mathrm{C}_{\mathrm{A} 0}}\right)\right)$
Open Calculator
ex $15.76923 \mathrm{~mol} / \mathrm{m}^{3} \mathrm{~s}=\left(\frac{80 \mathrm{~mol} / \mathrm{m}^{3}}{3 \mathrm{~s}}\right) \cdot\left(1-\exp \left(\left(-0.42 \mathrm{~s}^{-1}\right) \cdot 3 \mathrm{~s}\right)-\left(\frac{10 \mathrm{~mol} / \mathrm{m}^{3}}{80 \mathrm{~mol} / \mathrm{m}^{3}}\right)\right)$
21) Reactant Concentration for Two Steps First Order Reaction for Mixed Flow Reactor
$f \mathrm{f} \mathrm{C}_{\mathrm{k} 0}=\frac{\mathrm{C}_{\mathrm{A} 0}}{1+\left(\mathrm{k}_{\mathrm{I}} \cdot \tau_{\mathrm{m}}\right)}$
Open Calculator
ex $13.24503 \mathrm{~mol} / \mathrm{m}^{3}=\frac{80 \mathrm{~mol} / \mathrm{m}^{3}}{1+\left(0.42 \mathrm{~s}^{-1} \cdot 12 \mathrm{~s}\right)}$
22) Reactant Concentration in First Order followed by Zero Order Reaction
$f \mathrm{f} \mathrm{C}_{\mathrm{k} 0}=\mathrm{C}_{\mathrm{A} 0} \cdot \exp \left(-\mathrm{k}_{\mathrm{I}} \cdot \Delta \mathrm{t}\right)$
Open Calculator
ex $22.69232 \mathrm{~mol} / \mathrm{m}^{3}=80 \mathrm{~mol} / \mathrm{m}^{3} \cdot \exp \left(-0.42 \mathrm{~s}^{-1} \cdot 3 \mathrm{~s}\right)$
23) Time at Max Intermediate in First Order followed by Zero Order Reaction
$f \mathrm{x} \tau_{\mathrm{R}, \text { max }}=\left(\frac{1}{\mathrm{k}_{\mathrm{I}}}\right) \cdot \ln \left(\frac{\mathrm{k}_{\mathrm{I}} \cdot \mathrm{C}_{\mathrm{A} 0}}{\mathrm{k}_{0}}\right)$
Open Calculator
ex $3.911247 \mathrm{~s}=\left(\frac{1}{0.42 \mathrm{~s}^{-1}}\right) \cdot \ln \left(\frac{0.42 \mathrm{~s}^{-1} \cdot 80 \mathrm{~mol} / \mathrm{m}^{3}}{6.5 \mathrm{~mol} / \mathrm{m}^{3}{ }^{\mathrm{s}}}\right)$
24) Time at Maximum Intermediate Concentration for First Order Irreversible Reaction in Series
$\mathrm{fx}_{\tau_{R, \max }}=\frac{\ln \left(\frac{\mathrm{k}_{2}}{\mathrm{k}_{\mathrm{I}}}\right)}{\mathrm{k}_{2}-\mathrm{k}_{\mathrm{I}}}$
Open Calculator
ex $4.877141 \mathrm{~s}=\frac{\ln \left(\frac{0.08 \mathrm{~s}^{-1}}{0.42 \mathrm{~s}^{-1}}\right)}{0.08 \mathrm{~s}^{-1}-0.42 \mathrm{~s}^{-1}}$
25) Time at Maximum Intermediate Concentration for First Order Irreversible Reaction in Series in MFRE
$f \mathbf{x} \tau_{\mathrm{R}, \max }=\frac{1}{\sqrt{\mathrm{k}_{\mathrm{I}} \cdot \mathrm{k}_{2}}}$
ex $5.455447 \mathrm{~s}=\frac{1}{\sqrt{0.42 \mathrm{~s}^{-1} \cdot 0.08 \mathrm{~s}^{-1}}}$
26) Time Interval for First Order Reaction in First Order followed by Zero Order Reaction
$f \mathrm{x} \Delta \mathrm{t}=\left(\frac{1}{\mathrm{k}_{\mathrm{I}}}\right) \cdot \ln \left(\frac{\mathrm{C}_{\mathrm{A} 0}}{\mathrm{C}_{\mathrm{k} 0}}\right)$
ex $2.866602 \mathrm{~s}=\left(\frac{1}{0.42 \mathrm{~s}^{-1}}\right) \cdot \ln \left(\frac{80 \mathrm{~mol} / \mathrm{m}^{3}}{24 \mathrm{~mol} / \mathrm{m}^{3}}\right)$

## Variables Used

- $\mathbf{C}_{\mathbf{A O}}$ for $\mathbf{R}$ Initial Reactant Concentration using Intermediate (Mole per Cubic Meter)
- $\mathbf{C}_{\mathbf{A O}}$ Initial Reactant Concentration for Multiple Rxns (Mole per Cubic Meter)
- $\mathrm{C}_{\mathrm{AO}}$ Initial Reactant Concentration for Multiple Rxns (Mole per Cubic Meter)
- $\mathbf{C}_{\mathbf{k 0}}$ Reactant Concentration for Zero Order Series Rxn (Mole per Cubic Meter)
- $\mathrm{C}_{\mathrm{k} 0}$ Reactant Concentration for Zero Order Series Rxn (Mole per Cubic Meter)
- $\mathbf{C}_{\mathbf{k} 1}$ Reactant Concentration for 1st Order Series Rxns (Mole per Cubic Meter)
- $\mathbf{C}_{\mathbf{R}}$ Intermediate Concentration for Series Rxn (Mole per Cubic Meter)
- $\mathbf{C}_{\mathbf{R}}$ Intermediate Concentration for Series Rxn (Mole per Cubic Meter)
- $\mathbf{C}_{\mathbf{R}, 1 \text { st }}$ order Intermediate Conc. for 1st Order Series Rxn (Mole per Cubic Meter)
- $\mathbf{C}_{\mathbf{R}, \max }$ Maximum Intermediate Concentration (Mole per Cubic Meter)
- $\mathbf{C}_{\mathbf{R}, \max }$ Maximum Intermediate Concentration (Mole per Cubic Meter)
- C $\mathbf{S}_{\mathbf{S}}$ Final Product Concentration (Mole per Cubic Meter)
- $\mathbf{k}_{\mathbf{0}}$ Rate Constant for Zero Order Rxn for Multiple Rxns (Mole per Cubic Meter Second)
- $\mathbf{k}_{\mathbf{0}, \mathbf{k} \mathbf{1}}$ Rate Constant for Zero Order Rxn using k1 (Mole per Cubic Meter Second)
- $\mathbf{k}_{\mathbf{2}}$ Rate Constant for Second Step First Order Reaction (1 Per Second)
- $\mathbf{k}_{\mathbf{I}}$ Rate Constant for First Step First Order Reaction (1 Per Second)
- $\mathbf{k}_{\mathbf{I}}$ Rate Constant for First Step First Order Reaction (1 Per Second)
- $\Delta \mathbf{t}$ Time Interval for Multiple Reactions (Second)
- t Space Time for PFR (Second)
- $\mathbf{T}_{\mathbf{m}}$ Space Time for Mixed Flow Reactor (Second)
- $\mathbf{T}_{\mathbf{R}, \max }$ Time at Maximum Intermediate Concentration (Second)
- $\boldsymbol{T}_{\mathbf{R}, \max }$ Time at Maximum Intermediate Concentration (Second)


## Constants, Functions, Measurements used

- Function: $\exp , \exp ($ Number $)$

Exponential function

- Function: In, In(Number)

Natural logarithm function (base e)

- Function: sqrt, sqrt(Number)

Square root function

- Measurement: Time in Second (s)

Time Unit Conversion

- Measurement: Molar Concentration in Mole per Cubic Meter ( $\mathrm{mol} / \mathrm{m}^{3}$ ) Molar Concentration Unit Conversion
- Measurement: Reaction Rate in Mole per Cubic Meter Second ( $\mathrm{mol} / \mathrm{m}^{3 *} \mathrm{~s}$ ) Reaction Rate Unit Conversion《
- Measurement: First Order Reaction Rate Constant in 1 Per Second $\left(\mathrm{s}^{-1}\right)$ First Order Reaction Rate Constant Unit Conversion


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- Important Formulas in Design of Reactors \& Recycle Reactors for Single Reactions
- Important Formulas in Potpourri of Multiple Reactions
- Reactor Performance Equations for Constant Volume Reactions Formulas
- Reactor Performance Equations for Variable Volume Reactions Formulas

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