



Important Formulas in Potpourri of Multiple Reactions

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List of 26 Important Formulas in Potpourri of Multiple Reactions

Important Formulas in Potpourri of Multiple Reactions C

1) Initial Reactant Concentration for First Order Rxn for MFR using Intermediate Concentration 🕑

$$\mathbf{\hat{K}} \mathbf{C}_{\mathrm{A0}} = rac{\mathbf{C}_{\mathrm{R}} \cdot (1 + (\mathbf{k}_{\mathrm{I}} \cdot \mathbf{\tau}_{\mathrm{m}})) \cdot (1 + (\mathbf{k}_{2} \cdot \mathbf{\tau}_{\mathrm{m}}))}{\mathbf{k}_{\mathrm{I}} \cdot \mathbf{\tau}_{\mathrm{m}}}$$

$$\mathbf{23.48889 mol/m^{3}} = \frac{10 mol/m^{3} \cdot (1 + (0.42 s^{-1} \cdot 12 s)) \cdot (1 + (0.08 s^{-1} \cdot 12 s))}{0.42 s^{-1} \cdot 12 s}$$

2) Initial Reactant Concentration for First Order Rxn in MFR at Maximum Intermediate Concentration

$$\begin{aligned} & \mathbf{\hat{K}} \mathbf{C}_{A0} = \mathbf{C}_{\mathrm{R,max}} \cdot \left(\left(\left(\left(\frac{\mathbf{k}_2}{\mathbf{k}_{\mathrm{I}}} \right)^{\frac{1}{2}} \right) + 1 \right)^2 \right) \end{aligned}$$

$$\mathbf{ex} 82.53391 \mathrm{mol/m^3} = 40 \mathrm{mol/m^3} \cdot \left(\left(\left(\left(\frac{0.08 \mathrm{s^{-1}}}{0.42 \mathrm{s^{-1}}} \right)^{\frac{1}{2}} \right) + 1 \right)^2 \right) \end{aligned}$$

3) Initial Reactant Concentration for First Order Rxn in Series for Maximum Intermediate Concentration

$$\begin{aligned} & \textbf{K} \ \textbf{C}_{A0} = \frac{\textbf{C}_{R,max}}{\left(\frac{k_{I}}{k_{2}}\right)^{\frac{k_{2}}{k_{2}-k_{I}}}} \end{aligned} \\ & \textbf{ex} \ \textbf{59.08935mol/m^{3}} = \frac{40 \text{mol/m^{3}}}{\left(\frac{0.42 \text{s}^{-1}}{0.08 \text{s}^{-1}}\right)^{\frac{0.08 \text{s}^{-1}}{0.088^{-1}}}} \end{aligned}$$

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4) Initial Reactant Concentration for First Order Rxn in Series for MFR using Product Concentration

$$\begin{aligned} & \mathbf{\hat{fx}} \boxed{\mathbf{C}_{A0} = \frac{\mathbf{C}_{S} \cdot \left(1 + (\mathbf{k}_{I} \cdot \boldsymbol{\tau}_{m})\right) \cdot \left(1 + (\mathbf{k}_{2} \cdot \boldsymbol{\tau}_{m})\right)}{\mathbf{k}_{I} \cdot \mathbf{k}_{2} \cdot \left(\boldsymbol{\tau}_{m}^{2}\right)}} & & & & & \\ \\ & \mathbf{ex} \\ & 48.93519 \text{mol}/\text{m}^{3} = \frac{20 \text{mol}/\text{m}^{3} \cdot \left(1 + (0.42 \text{s}^{-1} \cdot 12 \text{s})\right) \cdot \left(1 + (0.08 \text{s}^{-1} \cdot 12 \text{s})\right)}{0.42 \text{s}^{-1} \cdot 0.08 \text{s}^{-1} \cdot \left((12 \text{s})^{2}\right)} \end{aligned}$$

5) Initial Reactant Concentration for Two Steps First Order Irreversible Reaction in Series 🖌

fx
$$C_{A0} = rac{C_{R} \cdot (k_2 - k_I)}{k_I \cdot (\exp(-k_I \cdot \tau) - \exp(-k_2 \cdot \tau))}$$

 $\underbrace{\texttt{ex}}_{89.23855 \text{mol}/\text{m}^3} = \frac{10 \text{mol}/\text{m}^3 \cdot (0.08 \text{s}^{-1} - 0.42 \text{s}^{-1})}{0.42 \text{s}^{-1} \cdot (\exp(-0.42 \text{s}^{-1} \cdot 30 \text{s}) - \exp(-0.08 \text{s}^{-1} \cdot 30 \text{s}))}$

6) Initial Reactant Concentration for Two Steps First Order Reaction for Mixed Flow Reactor 🚰

$$\begin{array}{l} & \textbf{fx} \ \hline C_{A0} = C_{k1} \cdot (1 + (k_{I} \cdot \tau_{m})) \end{array} \\ & \textbf{Open Calculator C} \\ & \textbf{ex} \ 80.332 mol/m^{3} = 13.3 mol/m^{3} \cdot (1 + (0.42 s^{-1} \cdot 12 s)) \end{array} \end{array}$$

7) Initial Reactant Concentration in First Order followed by Zero Order Reaction

fx
$$C_{A0} = rac{C_{k0}}{\exp(-k_{I}\cdot\Delta t)}$$

ex $84.61012 {
m mol}/{
m m^{3}} = rac{24 {
m mol}/{
m m^{3}}}{\exp(-0.42 {
m s}^{-1}\cdot3 {
m s})}$

8) Initial Reactant Concentration using Intermediate for First Order followed by Zero Order Reaction

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$$\mathbf{\hat{x}} \left[\mathrm{C}_{\mathrm{A0~for}~\mathrm{R}} = rac{\mathrm{C}_{\mathrm{R}} + (\mathrm{k}_{0} \cdot \Delta \mathrm{t})}{1 - \exp(-\mathrm{k}_{\mathrm{I}} \cdot \Delta \mathrm{t})}
ight]$$

$$\mathbf{41.18122 mol}/m^{3} = \frac{10 mol/m^{3} + (6.5 mol/m^{3} * s \cdot 3 s)}{1 - \exp(-0.42 s^{-1} \cdot 3 s)}$$



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9) Intermediate Concentration for First Order followed by Zero Order Reaction

fx
$$\left[\mathrm{C}_{\mathrm{R},\mathrm{1st \ order}} ~= \mathrm{C}_{\mathrm{A0}} \cdot \left(1 - \exp(-k_{\mathrm{I}} \cdot \Delta t) - \left(rac{\mathrm{k}_{\mathrm{0}} \cdot \Delta t}{\mathrm{C}_{\mathrm{A0}}}
ight)
ight)$$

 $\underbrace{ 37.80768 mol/m^3 = 80 mol/m^3 \cdot \left(1 - \exp(-0.42 s^{-1} \cdot 3 s) - \left(\frac{6.5 mol/m^3 * s \cdot 3 s}{80 mol/m^3} \right) \right) }$

10) Intermediate Concentration for First Order Reaction for Mixed Flow Reactor

$$\mathbf{\hat{k}} \mathbf{C}_{\mathrm{R}} = rac{\mathbf{C}_{\mathrm{A0}} \cdot \mathbf{k}_{\mathrm{I}} \cdot \mathbf{\tau}_{\mathrm{m}}}{\left(1 + \left(\mathbf{k}_{\mathrm{I}} \cdot \mathbf{\tau}_{\mathrm{m}}
ight)
ight) \cdot \left(1 + \left(\mathbf{k}_{2} \cdot \mathbf{\tau}_{\mathrm{m}}
ight)
ight)}$$

ex
$$34.05866 \text{mol}/\text{m}^3 = \frac{80 \text{mol}/\text{m}^3 \cdot 0.42 \text{s}^{-1} \cdot 12 \text{s}}{(1 + (0.42 \text{s}^{-1} \cdot 12 \text{s})) \cdot (1 + (0.08 \text{s}^{-1} \cdot 12 \text{s}))}$$

11) Intermediate Concentration for Two Steps First Order Irreversible Reaction in Series 💪

$$\mathbf{K} = \mathrm{C}_{\mathrm{A0}} \cdot \left(rac{\mathrm{k}_{\mathrm{I}}}{\mathrm{k}_{2} - \mathrm{k}_{\mathrm{I}}}
ight) \cdot \left(\exp(-\mathrm{k}_{\mathrm{I}} \cdot \mathbf{\tau}) - \exp(-\mathrm{k}_{2} \cdot \mathbf{\tau})
ight)$$

$$8.964735 \mathrm{mol}/\mathrm{m^{3}} = 80 \mathrm{mol}/\mathrm{m^{3}} \cdot \left(rac{0.42 \mathrm{s^{-1}}}{0.08 \mathrm{s^{-1}} - 0.42 \mathrm{s^{-1}}}
ight) \cdot \left(\exp(-0.42 \mathrm{s^{-1}} \cdot 30 \mathrm{s}) - \exp(-0.08 \mathrm{s^{-1}} \cdot 30 \mathrm{s})
ight)$$

12) Maximum Intermediate Concentration for First Order Irreversible Reaction in MFR 🕑

$$\begin{array}{l} & \\ & \\ \hline \mathbf{C}_{\mathrm{R,max}} = \frac{\mathbf{C}_{\mathrm{A0}}}{\left(\left(\left(\frac{k_2}{k_1}\right)^{\frac{1}{2}}\right) + 1\right)^2} \\ \\ & \\ & \\ & \\ \hline \mathbf{S}_{\mathrm{A0}} = \frac{80 \mathrm{mol/m^3}}{\left(\left(\left(\frac{0.08 \mathrm{s^{-1}}}{0.42 \mathrm{s^{-1}}}\right)^{\frac{1}{2}}\right) + 1\right)^2} \end{array}$$



ex



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13) Maximum Intermediate Concentration for First Order Irreversible Reaction in Series 🕑

fx
$$\left[\mathrm{C}_{\mathrm{R,max}} = \mathrm{C}_{\mathrm{A0}} \cdot \left(rac{\mathrm{k}_{\mathrm{I}}}{\mathrm{k}_{2}}
ight)^{rac{\mathrm{k}_{2}}{\mathrm{k}_{2}-\mathrm{k}_{\mathrm{I}}}}$$

$$\mathbf{54.15527 mol}/\mathrm{m^{3}} = 80 \mathrm{mol}/\mathrm{m^{3}} \cdot \left(\frac{0.42 \mathrm{s^{-1}}}{0.08 \mathrm{s^{-1}}}\right)^{\frac{0.08 \mathrm{s^{-1}}}{0.08 \mathrm{s^{-1}} - 0.42 \mathrm{s^{-1}}}}$$

14) Maximum Intermediate Concentration in First Order followed by Zero Order Reaction

fx
$$\left[\mathrm{C}_{\mathrm{R,max}} = \mathrm{C}_{\mathrm{A0}} \cdot \left(1 - \left(\frac{\mathrm{k}_0}{\mathrm{C}_{\mathrm{A0}} \cdot \mathrm{k}_\mathrm{I}} \cdot \left(1 - \ln\!\left(\frac{\mathrm{k}_0}{\mathrm{C}_{\mathrm{A0}} \cdot \mathrm{k}_\mathrm{I}} \right) \right) \right) \right)
ight)$$

$$39.1007 \text{mol}/\text{m}^{\scriptscriptstyle 3} = 80 \text{mol}/\text{m}^{\scriptscriptstyle 3} \cdot \left(1 - \left(\frac{6.5 \text{mol}/\text{m}^{\scriptscriptstyle 3} \ast \text{s}}{80 \text{mol}/\text{m}^{\scriptscriptstyle 3} \cdot 0.42 \text{s}^{\scriptscriptstyle -1}} \cdot \left(1 - \ln\!\left(\frac{6.5 \text{mol}/\text{m}^{\scriptscriptstyle 3} \ast \text{s}}{80 \text{mol}/\text{m}^{\scriptscriptstyle 3} \cdot 0.42 \text{s}^{\scriptscriptstyle -1}}\right)\right)\right)\right)$$

(12)

15) Product Concentration for First Order Reaction for Mixed Flow Reactor

$$\mathbf{fx} \boxed{\mathbf{C}_{\mathrm{S}} = \frac{\mathbf{C}_{\mathrm{A0}} \cdot \mathbf{k}_{\mathrm{I}} \cdot \mathbf{k}_{2} \cdot \left(\boldsymbol{\tau}_{\mathrm{m}}^{2}\right)}{\left(1 + \left(\mathbf{k}_{\mathrm{I}} \cdot \boldsymbol{\tau}_{\mathrm{m}}\right)\right) \cdot \left(1 + \left(\mathbf{k}_{2} \cdot \boldsymbol{\tau}_{\mathrm{m}}\right)\right)}}$$

$$\mathbf{ex} \ 32.69631 \text{mol}/\text{m}^{3} = \frac{80 \text{mol}/\text{m}^{3} \cdot 0.42 \text{s}^{-1} \cdot 0.08 \text{s}^{-1} \cdot ((12 \text{s})^{2})}{(1 + (0.42 \text{s}^{-1} \cdot 12 \text{s})) \cdot (1 + (0.08 \text{s}^{-1} \cdot 12 \text{s}))}$$

16) Rate Constant for First Order Reaction in First Order followed by Zero Order Reaction 🕑

fx
$$\mathbf{k}_{\mathrm{I}} = \left(\frac{1}{\Delta \mathrm{t}}\right) \cdot \ln\left(\frac{\mathrm{C}_{\mathrm{A0}}}{\mathrm{C}_{\mathrm{k0}}}\right)$$

ex $0.401324\mathrm{s}^{-1} = \left(\frac{1}{3\mathrm{s}}\right) \cdot \ln\left(\frac{80\mathrm{mol/m^{3}}}{24\mathrm{mol/m^{3}}}\right)$

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ex

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17) Rate Constant for First Order Reaction using Rate Constant for Zero Order Reaction

$$\mathbf{fx} \left[\mathbf{k}_{\mathrm{I}} = \left(rac{1}{\Delta \mathrm{t}}
ight) \cdot \ln \left(rac{\mathrm{C}_{\mathrm{A0}}}{\mathrm{C}_{\mathrm{A0}} - (\mathrm{k}_{\mathrm{0}} \cdot \Delta \mathrm{t}) - \mathrm{C}_{\mathrm{R}}}
ight)
ight]$$

$$\textbf{ex} \ 0.153351 \text{s}^{_{-1}} = \left(\frac{1}{3\text{s}}\right) \cdot \ln \left(\frac{80 \text{mol}/\text{m}^{_{3}}}{80 \text{mol}/\text{m}^{_{3}} - (6.5 \text{mol}/\text{m}^{_{3}}\text{*s} \cdot 3\text{s}) - 10 \text{mol}/\text{m}^{_{3}}}\right)$$

18) Rate Constant for First Step First Order Reaction for MFR at Maximum Intermediate Concentration

$$\begin{array}{l} \hbox{fx} \\ k_{I} = \frac{1}{k_{2} \cdot \left(\tau_{R,max}^{2}\right)} \\ \\ \hbox{ex} \\ 0.278458s^{-1} = \frac{1}{0.08s^{-1} \cdot \left((6.7s)^{2}\right)} \end{array}$$

19) Rate Constant for Second Step First Order Reaction for MFR at Maximum Intermediate Concentration

fx
$$k_2 = rac{1}{k_{\rm I} \cdot \left(au_{
m R,max}^2
ight)}$$
 ex $0.05304 {
m s}^{-1} = rac{1}{0.42 {
m s}^{-1} \cdot \left((6.7 {
m s})^2
ight)}$

20) Rate Constant for Zero Order Reaction using Rate Constant for First Order Reaction

$$\begin{split} & \overbrace{\mathbf{k}_{0,k1} = \left(\frac{C_{A0}}{\Delta t}\right) \cdot \left(1 - \exp((-k_{\rm I}) \cdot \Delta t) - \left(\frac{C_{\rm R}}{C_{A0}}\right)\right)}^{\text{Open Calculator C}} \\ & \underbrace{15.76923 \text{mol/m}^{3} \text{s} = \left(\frac{80 \text{mol/m}^{3}}{3 \text{s}}\right) \cdot \left(1 - \exp((-0.42 \text{s}^{-1}) \cdot 3 \text{s}) - \left(\frac{10 \text{mol/m}^{3}}{80 \text{mol/m}^{3}}\right)\right)}_{\text{Open Calculator C}} \end{split}$$



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21) Reactant Concentration for Two Steps First Order Reaction for Mixed Flow Reactor 💪 Open Calculator 🕑 $\mathbf{K} \mathbf{C}_{k0} = \frac{\mathbf{C}_{A0}}{1 + (\mathbf{k}_{L} \cdot \boldsymbol{\tau}_{m})}$ ex 13.24503 mol/m³ = $\frac{80$ mol/m³}{1 + (0.42s^{-1} \cdot 12s)} 22) Reactant Concentration in First Order followed by Zero Order Reaction 🕑 Open Calculator fx $C_{k0} = C_{A0} \cdot \exp(-k_{I} \cdot \Delta t)$ ex 22.69232mol/m³ = 80mol/m³ · exp(-0.42s⁻¹ · 3s) 23) Time at Max Intermediate in First Order followed by Zero Order Reaction Open Calculator $\mathbf{f} \mathbf{x} = \left(\frac{1}{\mathbf{k}_{\mathrm{I}}} \right) \cdot \ln \left(\frac{\mathbf{k}_{\mathrm{I}} \cdot \mathbf{C}_{\mathrm{A0}}}{\mathbf{k}_{\mathrm{O}}} \right)$ $\textbf{ex} \ 3.911247 \textbf{s} = \bigg(\frac{1}{0.42 \textbf{s}^{-1}}\bigg) \cdot \ln\bigg(\frac{0.42 \textbf{s}^{-1} \cdot 80 \textbf{mol}/\textbf{m}^3}{6.5 \textbf{mol}/\textbf{m}^3 * \textbf{s}}\bigg)$ 24) Time at Maximum Intermediate Concentration for First Order Irreversible Reaction in Series Open Calculator $au_{ m R,max} = rac{\ln\left(rac{k_2}{k_{ m I}} ight)}{k_2 - k_{ m T}}$

25) Time at Maximum Intermediate Concentration for First Order Irreversible Reaction in Series in





ex 4.877141s = $\frac{\ln\left(\frac{0.08s^{-1}}{0.42s^{-1}}\right)}{0.08s^{-1} - 0.42s^{-1}}$

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26) Time Interval for First Order Reaction in First Order followed by Zero Order Reaction 🚰

$$\begin{aligned} & \mathbf{\Delta t} = \left(\frac{1}{k_{\rm I}}\right) \cdot \ln\left(\frac{C_{\rm A0}}{C_{\rm k0}}\right) \\ \\ & \mathbf{Z}.866602 \mathrm{s} = \left(\frac{1}{0.42 \mathrm{s}^{-1}}\right) \cdot \ln\left(\frac{80 \mathrm{mol}/\mathrm{m}^{3}}{24 \mathrm{mol}/\mathrm{m}^{3}}\right) \end{aligned}$$





Variables Used

- CA0 for R Initial Reactant Concentration using Intermediate (Mole per Cubic Meter)
- C_{A0} Initial Reactant Concentration for Multiple Rxns (Mole per Cubic Meter)
- CA0 Initial Reactant Concentration for Multiple Rxns (Mole per Cubic Meter)
- C_{k0} Reactant Concentration for Zero Order Series Rxn (Mole per Cubic Meter)
- Ck0 Reactant Concentration for Zero Order Series Rxn (Mole per Cubic Meter)
- Ck1 Reactant Concentration for 1st Order Series Rxns (Mole per Cubic Meter)
- C_R Intermediate Concentration for Series Rxn (Mole per Cubic Meter)
- C_R Intermediate Concentration for Series Rxn (Mole per Cubic Meter)
- CR.1st order Intermediate Conc. for 1st Order Series Rxn (Mole per Cubic Meter)
- C_{R,max} Maximum Intermediate Concentration (Mole per Cubic Meter)
- C. C. Maximum Intermediate Concentration (Mole per Cubic Meter)
- **C**_S Final Product Concentration (Mole per Cubic Meter)
- k₀ Rate Constant for Zero Order Rxn for Multiple Rxns (Mole per Cubic Meter Second)
- k_{0,k1} Rate Constant for Zero Order Rxn using k1 (Mole per Cubic Meter Second)
- k2 Rate Constant for Second Step First Order Reaction (1 Per Second)
- k Rate Constant for First Step First Order Reaction (1 Per Second)
- k Rate Constant for First Step First Order Reaction (1 Per Second)
- Δt Time Interval for Multiple Reactions (Second)
- T Space Time for PFR (Second)
- T_m Space Time for Mixed Flow Reactor (Second)
- TR.max Time at Maximum Intermediate Concentration (Second)
- TR.max Time at Maximum Intermediate Concentration (Second)

Constants, Functions, Measurements used

- Function: exp, exp(Number) Exponential function
- Function: In, In(Number) Natural logarithm function (base e)
- Function: sqrt, sqrt(Number) Square root function
- Measurement: Time in Second (s) Time Unit Conversion
- Measurement: Molar Concentration in Mole per Cubic Meter (mol/m³) Molar Concentration Unit Conversion
- Measurement: Reaction Rate in Mole per Cubic Meter Second (mol/m^{3*}s) Reaction Rate Unit Conversion
- Measurement: First Order Reaction Rate Constant in 1 Per Second (s⁻¹) First Order Reaction Rate Constant Unit Conversion





Check other formula lists

- Basics of Chemical Reaction Engineering Formulas
- Basics of Parallel & Single Reactions
 Formulas
- Basics of Reactor Design and Temperature Recycle Reactors for Single Reactions Dependency from Arrhenius Law Formulas
 Important Formulas in Potpourri of Multiple
- Forms of Reaction Rate Formulas
- Important Formulas in Basics of Chemical Reaction Engineering & Forms of Reaction Rate
- Important Formulas in Constant and Variable Volume Batch Reactor

- Important Formulas in Constant Volume Batch Reactor for First, Second & Third Order Reaction
- Important Formulas in Design of Reactors & Recycle Reactors for Single Reactions
- Important Formulas in Potpourri of Multiple Reactions
- Reactor Performance Equations for Constant
 Volume Reactions Formulas
- Reactor Performance Equations for Variable
 Volume Reactions Formulas

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