



Orifices and Mouthpieces Formulas

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List of 33 Orifices and Mouthpieces Formulas

Orifices and Mouthpieces 2

Flow Head G

1) Absolute pressure head at constant head and atmospheric pressure head

 $\mathbf{K} \mathbf{H}_{\mathrm{AP}} = \mathbf{H}_{\mathrm{a}} + \mathbf{H}_{\mathrm{c}} - \left(\left(\left(rac{\mathbf{V}_{\mathrm{o}}}{0.62}
ight)^2
ight) \cdot \left(rac{1}{2 \cdot 9.81}
ight)
ight)$

Open Calculator 🗗

$$\boxed{13.48909\mathrm{m} = 7\mathrm{m} + 10.5\mathrm{m} - \left(\left(\left(\frac{5.5\mathrm{m/s}}{0.62}\right)^2\right) \cdot \left(\frac{1}{2 \cdot 9.81}\right)\right)}$$

2) Atmospheric pressure head at constant head and absolute pressure head

 $\mathbf{H}_{\mathrm{a}} = \mathbf{H}_{\mathrm{AP}} - \mathbf{H}_{\mathrm{c}} + \left(\left(\left(\frac{\mathbf{V}_{\mathrm{o}}}{0.62} \right)^2 \right) \cdot \left(\frac{1}{2 \cdot 9.81} \right) \right)$

Open Calculator

$$\boxed{7.510911 \text{m} = 14 \text{m} - 10.5 \text{m} + \left(\left(\left(\frac{5.5 \text{m/s}}{0.62} \right)^2 \right) \cdot \left(\frac{1}{2 \cdot 9.81} \right) \right) }$$

3) Head of Liquid above Centre of Orifice

 $H = rac{V_{
m th}^2}{2 \cdot 9.81}$

Open Calculator

$$4.12844 \text{m} = \frac{(9 \text{m/s})^2}{2 \cdot 9.81}$$

4) Head of liquid for head loss and coefficient of velocity

 $\mathrm{H}=rac{\mathrm{h_f}}{1-\left(\mathrm{C_v^2}
ight)}$

Open Calculator 🗗

5) Loss of head due to fluid resistance

$$\mathbf{f}\mathbf{x} igg[\mathbf{h}_{\mathrm{f}} = \mathbf{H} \cdot ig(1 - ig(\mathbf{C}_{\mathrm{v}}^2 ig) ig) ig]$$

Open Calculator

$$\boxed{\mathbf{ex}} \left[0.768 \mathrm{m} = 5 \mathrm{m} \cdot \left(1 - \left(\left(0.92 \right)^2 \right) \right) \right]$$

6) Loss of head due to sudden enlargement

$$\mathbf{h}_{\mathrm{L}} = rac{\left(V_{\mathrm{i}} - V_{\mathrm{o}}
ight)^2}{2 \cdot 9.81}$$

Open Calculator

Flow Rate

7) Coefficient of discharge

$$\boxed{\text{fx}} C_d = \frac{Q_a}{Q_{th}}$$

Open Calculator

$$\boxed{0.875 = \frac{0.7 \text{m}^3/\text{s}}{0.8 \text{m}^3/\text{s}}}$$

8) Coefficient of discharge for area and velocity

$$\mathbf{K} \mathbf{C}_{\mathrm{d}} = rac{\mathbf{v}_{\mathrm{a}} \cdot \mathbf{A}_{\mathrm{a}}}{\mathbf{V}_{\mathrm{th}} \cdot \mathbf{A}_{\mathrm{t}}}$$

Open Calculator 🗗

ex
$$0.820513 = rac{8 ext{m/s} \cdot 4.80 ext{m}^2}{9 ext{m/s} \cdot 5.2 ext{m}^2}$$

9) Coefficient of Discharge given Time for Emptying Tank

$$\mathbf{K} \mathbf{C}_{\mathrm{d}} = rac{2 \cdot A_{\mathrm{T}} \cdot \left(\left(\sqrt{H_{\mathrm{i}}}
ight) - \left(\sqrt{H_{\mathrm{f}}}
ight)
ight)}{t_{\mathrm{total}} \cdot a \cdot \sqrt{2 \cdot 9.81}}$$

Open Calculator 🗗

$$\boxed{\textbf{ex}} 0.786502 = \frac{2 \cdot 1144 \text{m}^2 \cdot \left(\left(\sqrt{24 \text{m}}\right) - \left(\sqrt{20.1 \text{m}}\right)\right)}{30 \text{s} \cdot 9.1 \text{m}^2 \cdot \sqrt{2 \cdot 9.81}}$$



10) Coefficient of Discharge given Time of Emptying Circular Horizontal Tank

 $\mathbf{K} \mathbf{C}_{\mathrm{d}} = rac{4 \cdot \mathrm{L} \cdot \left(\left(\left(\left(\left(2 \cdot \mathrm{r_{1}}
ight) - \mathrm{H_{f}}
ight)^{rac{3}{2}}
ight) - \left(\left(2 \cdot \mathrm{r_{1}}
ight) - \mathrm{H_{i}}
ight)^{rac{3}{2}}
ight)}{3 \cdot \mathrm{t_{total}} \cdot \mathrm{a} \cdot \left(\sqrt{2 \cdot 9.81}
ight)}$

Open Calculator

Open Calculator

$$\boxed{0.892776 = \frac{4 \cdot 31 m \cdot \left(\left(\left((2 \cdot 21 m\right) - 20.1 m\right)^{\frac{3}{2}}\right) - \left((2 \cdot 21 m) - 24 m\right)^{\frac{3}{2}}\right)}{3 \cdot 30 s \cdot 9.1 m^2 \cdot \left(\sqrt{2 \cdot 9.81}\right)}}$$

11) Coefficient of Discharge given Time of Emptying Hemispherical Tank

 $\mathbf{R} = \frac{\pi \cdot \left(\left(\left(\frac{4}{3} \right) \cdot \mathbf{R_t} \cdot \left(\left(\mathbf{H_i}^{\frac{3}{2}} \right) - \left(\mathbf{H_f}^{\frac{3}{2}} \right) \right) \right) - \left(\left(\frac{2}{5} \right) \cdot \left(\left(\mathbf{H_i}^{\frac{5}{2}} \right) - \left(\mathbf{H_f} \right)^{\frac{5}{2}} \right) \right) \right)}{\mathbf{R}}$

 $\underbrace{ 0.376754 = \frac{\pi \cdot \left(\left(\left(\frac{4}{3} \right) \cdot 15 \text{m} \cdot \left(\left((24 \text{m})^{\frac{3}{2}} \right) - \left((20.1 \text{m})^{\frac{3}{2}} \right) \right) \right) - \left(\left(\frac{2}{5} \right) \cdot \left(\left((24 \text{m})^{\frac{5}{2}} \right) - (20.1 \text{m})^{\frac{5}{2}} \right) \right) \right) }_{30 \text{s} \cdot 9.1 \text{m}^2 \cdot \left(\sqrt{2 \cdot 9.81} \right) } }$

 $t_{total} \cdot a \cdot \left(\sqrt{2 \cdot 9.81}\right)$

12) Discharge in Borda's Mouthpiece Running Free

 $extbf{K} Q_{ ext{M}} = 0.5 \cdot ext{A} \cdot \sqrt{2 \cdot 9.81 \cdot ext{H}_{ ext{c}}}$

Open Calculator

- ex $36.60027 \mathrm{m}^3/\mathrm{s} = 0.5 \cdot 5.1 \mathrm{m}^2 \cdot \sqrt{2 \cdot 9.81 \cdot 10.5 \mathrm{m}}$
- 13) Discharge in Borda's Mouthpiece Running Full 🖸

 $\mathbf{Q}_{\mathrm{M}} = 0.707 \cdot \mathrm{A} \cdot \sqrt{2 \cdot 9.81 \cdot \mathrm{H_c}}$

Open Calculator 🗗

- ex $51.75279 \mathrm{m}^3/\mathrm{s} = 0.707 \cdot 5.1 \mathrm{m}^2 \cdot \sqrt{2 \cdot 9.81 \cdot 10.5 \mathrm{m}}$
- 14) Discharge in Convergent-Divergent Mouthpiece

 $\left[\mathrm{Q_{M}} = \mathrm{a_{c}} \cdot \sqrt{2 \cdot 9.81 \cdot \mathrm{H_{c}}}
ight]$

Open Calculator 🚰

- $\texttt{ex} \, \boxed{30.1414 \text{m}^3/\text{s} = 2.1 \text{m}^2 \cdot \sqrt{2 \cdot 9.81 \cdot 10.5 \text{m}}}$
- 15) Discharge through fully sub-merged orifice 🖸

 $\left|\mathbf{Q}_{\mathrm{O}}=\mathrm{C}_{\mathrm{d}}\cdot\mathrm{w}\cdot\left(\mathrm{H}_{\mathrm{b}}-\mathrm{H}_{\mathrm{top}}
ight)\cdot\left(\sqrt{2\cdot9.81\cdot\mathrm{H}_{\mathrm{L}}}
ight)$

Open Calculator 🗗

 $= 19.07444 m^3/s = 0.87 \cdot 3.5 m \cdot (20m - 19.9m) \cdot \left(\sqrt{2 \cdot 9.81 \cdot 200m}\right)$



16) Discharge through large rectangular orifice G

 $\mathbf{K} \ \mathrm{Q}_{\mathrm{O}} = \left(rac{2}{3}
ight) \cdot \mathrm{C}_{\mathrm{d}} \cdot \mathrm{b} \cdot \left(\sqrt{2 \cdot 9.81}
ight) \cdot \left(\left(\mathrm{H}_{\mathrm{b}}^{1.5}
ight) - \left(\mathrm{H}_{\mathrm{top}}^{1.5}
ight)
ight)$

Open Calculator 2

 $\boxed{\textbf{ex}} 20.65482 \text{m}^{_{3}}/\text{s} = \left(\frac{2}{3}\right) \cdot 0.87 \cdot 12 \text{m} \cdot \left(\sqrt{2 \cdot 9.81}\right) \cdot \left(\left((20 \text{m})^{1.5}\right) - \left((19.9 \text{m})^{1.5}\right)\right)$

17) Discharge through partially sub-merged orifice G

Open Calculator

$$\mathrm{Q_{O}} = \left(\mathrm{C_{d} \cdot w \cdot (H_{b} - H_{L}) \cdot \left(\sqrt{2 \cdot 9.81 \cdot H_{L}}
ight)}
ight) + \left(\left(rac{2}{3}
ight) \cdot \mathrm{C_{d} \cdot b \cdot \left(\sqrt{2 \cdot 9.81}
ight) \cdot \left(\left(H_{L}^{1.5}
ight) - H_{L}^{1.5}
ight)}
ight) + \left(\left(rac{2}{3}
ight) \cdot \mathrm{C_{d} \cdot b \cdot \left(\sqrt{2 \cdot 9.81}
ight) \cdot \left(\left(H_{L}^{1.5}
ight) - H_{L}^{1.5}
ight)}
ight) + \left(\left(rac{2}{3}
ight) \cdot \mathrm{C_{d} \cdot b \cdot \left(\sqrt{2 \cdot 9.81}
ight) \cdot \left(\left(H_{L}^{1.5}
ight) - H_{L}^{1.5}
ight)}
ight) + \left(\left(H_{L}^{1.5}
ight) - H_{L}^{1.5}
ight) \cdot \left(H_{L}^{1.5}
ight) - H_{L}^{1.5}
ight) + H_{L}^{1.5}$$

ex

Geometric Dimensions

18) Area at vena contracta for discharge and constant head

 $\mathbf{a}_{\mathrm{c}} = rac{Q_{\mathrm{M}}}{\sqrt{2\cdot 9.81\cdot \mathrm{H_{c}}}}$

Open Calculator

ex
$$2.104083 \mathrm{m}^2 = \frac{30.2 \mathrm{m}^3/\mathrm{s}}{\sqrt{2 \cdot 9.81 \cdot 10.5 \mathrm{m}}}$$

19) Area of Mouthpiece in Borda's Mouthpiece Running Free

 $A = \frac{Q_{\rm M}}{0.5 \cdot \sqrt{2 \cdot 9.81 \cdot H_{\rm o}}}$

Open Calculator

$$\boxed{\text{ex}} 4.208165 m^2 = \frac{30.2 m^3/s}{0.5 \cdot \sqrt{2 \cdot 9.81 \cdot 10.5 m}}$$

20) Area of Mouthpiece in Borda's Mouthpiece Running Full 🗗

$$A = rac{Q_{M}}{0.707 \cdot \sqrt{2 \cdot 9.81 \cdot H_{c}}}$$

Open Calculator 🚰

$$2.976072 \text{m}^2 = \frac{30.2 \text{m}^3/\text{s}}{0.707 \cdot \sqrt{2 \cdot 9.81 \cdot 10.5 \text{m}}}$$





21) Area of Orifice given Time of Emptying Hemispherical Tank

 $a = \frac{\pi \cdot \left(\left(\left(\frac{4}{3}\right) \cdot R_t \cdot \left(\left(H_i^{\frac{3}{2}}\right) - \left(H_f^{\frac{3}{2}}\right)\right)\right) - \left(\left(\frac{2}{5}\right) \cdot \left(\left(H_i^{\frac{5}{2}}\right) - \left(H_f\right)^{\frac{5}{2}}\right)\right)\right)}{t_{total} \cdot C_d \cdot \left(\sqrt{2 \cdot 9.81}\right)}$

Open Calculator

$$\mathbf{t}_{ ext{total}} \cdot \mathrm{C}_{ ext{d}} \cdot \left(\sqrt{2 \cdot 9.81}
ight)$$

$$3.940758 \text{m}^2 = \frac{\pi \cdot \left(\left(\left(\frac{4}{3} \right) \cdot 15 \text{m} \cdot \left(\left((24 \text{m})^{\frac{3}{2}} \right) - \left((20.1 \text{m})^{\frac{3}{2}} \right) \right) \right) - \left(\left(\frac{2}{5} \right) \cdot \left(\left((24 \text{m})^{\frac{5}{2}} \right) - (20.1 \text{m})^{\frac{5}{2}} \right) \right) \right)}{30 \text{s} \cdot 0.87 \cdot \left(\sqrt{2 \cdot 9.81} \right)}$$

22) Area of Tank given Time for Emptying Tank

 $oldsymbol{\mathbb{A}} \mathbf{A}_{\mathrm{T}} = rac{\mathbf{t}_{\mathrm{total}} \cdot \mathbf{C}_{\mathrm{d}} \cdot \mathbf{a} \cdot \left(\sqrt{2 \cdot 9.81}
ight)}{2 \cdot \left(\left(\sqrt{\mathrm{H}_{\mathrm{i}}}
ight) - \left(\sqrt{\mathrm{H}_{\mathrm{f}}}
ight)
ight)}$

Open Calculator 2

23) Coefficient of Contraction given Area of Orifice

 $C_{c} = \frac{A_{c}}{a}$

Open Calculator 🚰

24) Horizontal distance for coefficient of velocity and vertical distance 🗗

 $\mathbf{R} = \mathrm{C_v} \cdot \left(\sqrt{4 \cdot \mathrm{V} \cdot \mathrm{H}}\right)$

Open Calculator

25) Vertical distance for coefficient of velocity and horizontal distance 🖒

 $V = \frac{R^2}{4 \cdot (C_-^2) \cdot H}$

Open Calculator 🚰





Velocity and Time

26) Coefficient of velocity

fx
$$C_{
m v} = rac{v_{
m a}}{V_{
m th}}$$

$$0.888889 = \frac{8 \text{m/s}}{9 \text{m/s}}$$

27) Coefficient of velocity for horizontal and vertical distance

$$\mathrm{C_v} = rac{\mathrm{R}}{\sqrt{4\cdot\mathrm{V}\cdot\mathrm{H}}}$$

$$2.571478 = \frac{23\mathrm{m}}{\sqrt{4\cdot4\mathrm{m}\cdot5\mathrm{m}}}$$

28) Coefficient of Velocity given Head Loss

$$\boxed{ \text{fc} \left[C_v = \sqrt{1 - \left(\frac{h_f}{H} \right)} \right] }$$

29) Theoretical velocity 🔓

$$v = \sqrt{2 \cdot 9.81 \cdot H_p}$$

ex
$$28.7061 \text{m/s} = \sqrt{2 \cdot 9.81 \cdot 42 \text{m}}$$

30) Time of Emptying Circular Horizontal Tank

$$\boxed{\textbf{t}_{total} = \frac{4 \cdot L \cdot \left(\left(\left((2 \cdot r_1) - H_f \right)^{\frac{3}{2}} \right) - \left((2 \cdot r_1) - H_i \right)^{\frac{3}{2}} \right)}{3 \cdot C_d \cdot a \cdot \left(\sqrt{2 \cdot 9.81} \right)}}$$





31) Time of Emptying Hemispherical Tank 🗗

 $\boxed{\textbf{t}_{total} = \frac{\pi \cdot \left(\left(\left(\frac{4}{3}\right) \cdot R_t \cdot \left(\left(H_i^{1.5}\right) - \left(H_f^{1.5}\right)\right)\right) - \left(0.4 \cdot \left(\left(H_i^{\frac{5}{2}}\right) - \left(H_f\right)^{\frac{5}{2}}\right)\right)\right)}{C_d \cdot a \cdot \left(\sqrt{2 \cdot 9.81}\right)}}$

Open Calculator

 $= \frac{\pi \cdot \left(\left(\left(\frac{4}{3} \right) \cdot 15 \text{m} \cdot \left(\left((24 \text{m})^{1.5} \right) - \left((20.1 \text{m})^{1.5} \right) \right) \right) - \left(0.4 \cdot \left(\left((24 \text{m})^{\frac{5}{2}} \right) - (20.1 \text{m})^{\frac{5}{2}} \right) \right) \right)}{0.87 \cdot 9.1 \text{m}^2 \cdot \left(\sqrt{2 \cdot 9.81} \right) }$

32) Time of Emptying Tank through Orifice at Bottom

 $oldsymbol{t_{total}} = rac{2 \cdot A_T \cdot \left(\left(\sqrt{H_i}
ight) - \left(\sqrt{H_f}
ight)
ight)}{C_d \cdot a \cdot \sqrt{2 \cdot 9.81}}$

Open Calculator

33) Velocity of liquid at C-C for Hc, Ha, and H

 $\left| V_{\mathrm{i}} = \sqrt{2 \cdot 9.81 \cdot \left(\mathrm{H_a} + \mathrm{H_c} - \mathrm{H_{AP}}
ight)}
ight|$

Open Calculator

ex $8.286736 \text{m/s} = \sqrt{2 \cdot 9.81 \cdot (7 \text{m} + 10.5 \text{m} - 14 \text{m})}$



Variables Used

- a Area of Orifice (Square Meter)
- A Area (Square Meter)
- Aa Actual Area (Square Meter)
- ac Area at Vena Contracta (Square Meter)
- A_c Area of Jet (Square Meter)
- At Theoretical Area (Square Meter)
- AT Area of Tank (Square Meter)
- **b** Thickness of Dam (Meter)
- C_c Coefficient of Contraction
- C_d Coefficient of Discharge
- C_v Coefficient of Velocity
- H Head of the Liquid (Meter)
- Ha Atmospheric Pressure Head (Meter)
- H_{AP} Absolute Pressure Head (Meter)
- H_b Height of Liquid Bottom Edge (Meter)
- H_c Constant Head (Meter)
- **h**_f Head Loss (Meter)
- **H**_f Final Height of Liquid (Meter)
- Hi Initial Height of Liquid (Meter)
- h_L Loss of Head (Meter)
- **H**_L Difference in Liquid Level (Meter)
- H_p Pelton Head (Meter)
- H_{top} Height of Liquid Top Edge (Meter)
- L Length (Meter)
- Qa Actual Discharge (Cubic Meter per Second)
- Q_M Discharge through Mouthpiece (Cubic Meter per Second)
- Q_O Discharge through Orifice (Cubic Meter per Second)
- Q_{th} Theoretical Discharge (Cubic Meter per Second)
- R Horizontal Distance (Meter)
- r₁ Radius (Meter)
- R_t Hemispherical Tank Radius (Meter)
- t_{total} Total Time Taken (Second)
- V Velocity (Meter per Second)





- **V** Vertical Distance (Meter)
- Va Actual Velocity (Meter per Second)
- V_i Velocity of Liquid Inlet (Meter per Second)
- V_o Velocity of Liquid Outlet (Meter per Second)
- V_{th} Theoretical Velocity (Meter per Second)
- w Width (Meter)





Constants, Functions, Measurements used

- Constant: pi, 3.14159265358979323846264338327950288
 Archimedes' constant
- Function: sqrt, sqrt(Number)

A square root function is a function that takes a non-negative number as an input and returns the square root of the given input number.

- Measurement: Length in Meter (m)
 Length Unit Conversion
- Measurement: Time in Second (s)

 Time Unit Conversion
- Measurement: Area in Square Meter (m²)

 Area Unit Conversion
- Measurement: Speed in Meter per Second (m/s) Speed Unit Conversion
- Measurement: Volumetric Flow Rate in Cubic Meter per Second (m³/s) Volumetric Flow Rate Unit Conversion





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