



Steady State Heat Conduction with Heat Generation Formulas

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List of 14 Steady State Heat Conduction with Heat Generation **Formulas**

Steady State Heat Conduction with Heat Generation &

1) Location of Maximum Temperature in Plane Wall with Symmetrical Boundary Conditions

$$X = rac{b}{2}$$

Open Calculator 🚰

$$= \frac{12.601905 \text{m}}{2}$$

2) Maximum Temperature in Plane Wall Surrounded by Fluid with Symmetrical Boundary Conditions 🗗

$$\mathbf{f}_{max} = rac{q_G \cdot b^2}{8 \cdot k} + rac{q_G \cdot b}{2 \cdot h_c} + T_{\infty}$$

Open Calculator 2

$$\boxed{ 549.4162 K = \frac{100 W/m^3 \cdot (12.601905 m)^2}{8 \cdot 10.18 W/(m^* K)} + \frac{100 W/m^3 \cdot 12.601905 m}{2 \cdot 1.834786 W/m^2 K} + 11 K }$$

3) Maximum Temperature in Plane Wall with Symmetrical Boundary Conditions

$$T_{
m max} = T_1 + rac{{
m q_G} \cdot {
m b}^2}{8 \cdot {
m k}}$$

Open Calculator

$$= 500 \text{K} = 305 \text{K} + \frac{100 \text{W/m}^3 \cdot (12.601905 \text{m})^2}{8 \cdot 10.18 \text{W/(m*K)}}$$

4) Maximum Temperature in Solid Cylinder G

$$oxed{T_{ ext{max}} = T_{ ext{w}} + rac{ ext{q}_{ ext{G}} \cdot ext{R}_{ ext{cy}}^2}{4 \cdot ext{k}}}$$

Open Calculator

$$= 273 \text{K} + \frac{100 \text{W/m}^3 \cdot (9.61428 \text{m})^2}{4 \cdot 10.18 \text{W/(m*K)} }$$

5) Maximum Temperature in Solid Sphere 🗗

$$T_{
m max} = T_{
m w} + rac{{
m q}_{
m G} \cdot R_{
m s}^2}{6 \cdot {
m k}}$$

Open Calculator

$$= 273 \text{K} + \frac{100 \text{W/m}^3 \cdot (11.775042 \text{m})^2}{6 \cdot 10.18 \text{W/(m*K)}}$$





6) Maximum Temperature Inside Solid Cylinder Immersed in Fluid

 $T_{max} = T_{\infty} + rac{q_G \cdot R_{cy} \cdot \left(2 + rac{h_c \cdot R_{cy}}{k}
ight)}{4 \cdot h_c}$

Open Calculator 🗗

$$\frac{4 \cdot h_c}{4 \cdot h_c}$$

$$\boxed{ \begin{aligned} \text{ex} \\ 500\text{K} &= 11\text{K} + \frac{100\text{W}/\text{m}^3 \cdot 9.61428\text{m} \cdot \left(2 + \frac{1.834786\text{W}/\text{m}^2\text{*K} \cdot 9.61428\text{m}}{10.18\text{W}/(\text{m}^*\text{K})}\right) \\ &\quad 4 \cdot 1.834786\text{W}/\text{m}^2\text{*K} \end{aligned} }$$

7) Surface Temperature of Solid Cylinder Immersed in Fluid

$$\left[T_{
m w} = T_{\infty} + rac{{
m q}_{
m G} \cdot {
m R}_{
m cy}}{2 \cdot {
m h}_{
m c}}
ight]$$

Open Calculator

$$\begin{array}{c} \text{ex} \\ 273 \text{K} = 11 \text{K} + \frac{100 \text{W/m}^3 \cdot 9.61428 \text{m}}{2 \cdot 1.834786 \text{W/m}^2 \text{*K}} \end{array}$$

8) Temperature at given Thickness x Inside Plane Wall Surrounded by Fluid

$$T = rac{q_G}{8 \cdot k} \cdot \left(b^2 - 4 \cdot x^2
ight) + rac{q_G \cdot b}{2 \cdot h_c} + T_{\infty}$$

Open Calculator 🚰

$$\boxed{\text{ex}} \left[460 \text{K} = \frac{100 \text{W/m}^3}{8 \cdot 10.18 \text{W/(m*K)}} \cdot \left((12.601905 \text{m})^2 - 4 \cdot (4.266748 \text{m})^2 \right) + \frac{100 \text{W/m}^3 \cdot 12.601905 \text{m}}{2 \cdot 1.834786 \text{W/m}^2 * \text{K}} + 11 \text{K} \right] \right] + \frac{100 \text{W/m}}{2 \cdot 1.834786 \text{W/m}^2 * \text{K}} + 11 \text{K} + 11$$

9) Temperature Inside Hollow Cylinder at given Radius between Inner and Outer Radius 🗲

$$T = rac{q_G}{4 \cdot k} \cdot \left(r_o^2 - r^2
ight) + T_o + rac{\ln\left(rac{r}{r_o}
ight)}{\ln\left(rac{r_o}{r_i}
ight)} \cdot \left(rac{q_G}{4 \cdot k} \cdot \left(r_o^2 - r_i^2
ight) + \left(T_o - T_i
ight)
ight)$$

Open Calculator

open Calculator

$$\boxed{460 \text{K} = \frac{100 \text{W/m}^3}{4 \cdot 10.18 \text{W/(m*K)}} \cdot \left((30.18263 \text{m})^2 - (4 \text{m})^2 \right) + 300 \text{K} + \frac{\ln \left(\frac{4 \text{m}}{30.18263 \text{m}} \right)}{\ln \left(\frac{30.18263 \text{m}}{2.5 \text{m}} \right)} \cdot \left(\frac{100 \text{W/m}^3}{4 \cdot 10.18 \text{W/(m*K)}} \cdot \left((30.18263 \text{m})^2 - (4 \text{m})^2 \right) \right) + 300 \text{K} + \frac{\ln \left(\frac{4 \text{m}}{30.18263 \text{m}} \right)}{\ln \left(\frac{30.18263 \text{m}}{2.5 \text{m}} \right)} \cdot \left(\frac{100 \text{W/m}^3}{4 \cdot 10.18 \text{W/(m*K)}} \cdot \left((30.18263 \text{m})^2 - (4 \text{m})^2 \right) \right) + 300 \text{K} + \frac{\ln \left(\frac{4 \text{m}}{30.18263 \text{m}} \right)}{\ln \left(\frac{30.18263 \text{m}}{2.5 \text{m}} \right)} \cdot \left(\frac{100 \text{W/m}^3}{4 \cdot 10.18 \text{W/(m*K)}} \cdot \left((30.18263 \text{m})^2 - (4 \text{m})^2 \right) \right) + 300 \text{K} + \frac{\ln \left(\frac{4 \text{m}}{30.18263 \text{m}} \right)}{\ln \left(\frac{30.18263 \text{m}}{2.5 \text{m}} \right)} \cdot \left(\frac{100 \text{W/m}^3}{4 \cdot 10.18 \text{W/(m*K)}} \cdot \left((30.18263 \text{m})^2 - (4 \text{m})^2 \right) \right) + 300 \text{W/m}^3}$$

10) Temperature Inside Hollow Sphere at given Radius between Inner and Outer Radius 🖸

$$T = T_{\mathrm{w}} + rac{q_{\mathrm{G}}}{6 \cdot \mathrm{k}} \cdot \left(\mathrm{r}_{2}^{2} - \mathrm{r}^{2}
ight) + rac{q_{\mathrm{G}} \cdot \mathrm{r}_{1}^{3}}{3 \cdot \mathrm{k}} \cdot \left(rac{1}{\mathrm{r}_{2}} - rac{1}{\mathrm{r}}
ight)$$

Open Calculator 🚰

$$\boxed{ 460 \text{K} = 273 \text{K} + \frac{100 \text{W/m}^3}{6 \cdot 10.18 \text{W/(m*K)}} \cdot \left(\left(2 \text{m}\right)^2 - \left(4 \text{m}\right)^2 \right) + \frac{100 \text{W/m}^3 \cdot \left(6.320027 \text{m}\right)^3}{3 \cdot 10.18 \text{W/(m*K)}} \cdot \left(\frac{1}{2 \text{m}} - \frac{1}{4 \text{m}} \right)^2 \right) }$$



11) Temperature Inside Plane Wall at given Thickness x with Symmetrical Boundary Conditions

 \mathbf{k} $\mathbf{t}_1 = -rac{\mathbf{q}_{\mathrm{G}}\cdot\mathbf{b}^2}{2\cdot\mathbf{k}}\cdot\left(rac{\mathbf{x}}{\mathbf{b}}-\left(rac{\mathbf{x}}{\mathbf{b}}
ight)^2
ight)+\mathrm{T}_1$

Open Calculator

$$= 130.3241 \text{K} = -\frac{100 \text{W/m}^3 \cdot (12.601905 \text{m})^2}{2 \cdot 10.18 \text{W/(m*K)}} \cdot \left(\frac{4.266748 \text{m}}{12.601905 \text{m}} - \left(\frac{4.266748 \text{m}}{12.601905 \text{m}} \right)^2 \right) + 305 \text{K}$$

12) Temperature Inside Solid Cylinder at given Radius

$$t = rac{q_G}{4 \cdot k} \cdot \left(R_{cy}^2 - r^2
ight) + T_w$$

Open Calculator

$$\boxed{ 460.7072 \text{K} = \frac{100 \text{W/m}^3}{4 \cdot 10.18 \text{W/(m*K)}} \cdot \left(\left(9.61428 \text{m} \right)^2 - \left(4 \text{m} \right)^2 \right) + 273 \text{K} }$$

13) Temperature Inside Solid Cylinder at given Radius Immersed in Fluid

$$\boxed{\mathbf{fz} \left[t = \frac{q_G}{4 \cdot k} \cdot \left(R_{cy}^2 - r^2 \right) + T_\infty + \frac{q_G \cdot R_{cy}}{2 \cdot h_c} \right]}$$

Open Calculator

$$\boxed{ 460.7073 \text{K} = \frac{100 \text{W/m}^3}{4 \cdot 10.18 \text{W/(m*K)}} \cdot \left(\left(9.61428 \text{m} \right)^2 - \left(4 \text{m} \right)^2 \right) + 11 \text{K} + \frac{100 \text{W/m}^3 \cdot 9.61428 \text{m}}{2 \cdot 1.834786 \text{W/m}^2 \text{K}} }$$

14) Temperature Inside Solid Sphere at given Radius

$$\mathbf{fz} \left[\mathrm{t_2} = \mathrm{T_w} + rac{\mathrm{q_G}}{6 \cdot \mathrm{k}} \cdot \left(\mathrm{R_s^2} - \mathrm{r^2}
ight)
ight]$$

Open Calculator

$$\boxed{ 473.8049 \text{K} = 273 \text{K} + \frac{100 \text{W/m}^3}{6 \cdot 10.18 \text{W/(m*K)}} \cdot \left((11.775042 \text{m})^2 - (4 \text{m})^2 \right) }$$



Variables Used

- **b** Wall Thickness (Meter)
- **h**_c Convection Heat Transfer Coefficient (Watt per Square Meter per Kelvin)
- **k** Thermal Conductivity (Watt per Meter per K)
- **q**_G Internal Heat Generation (Watt Per Cubic Meter)
- r Radius (Meter)
- r₁ Inner Radius of Sphere (Meter)
- r2 Outer Radius of Sphere (Meter)
- R_{cv} Radius of Cylinder (Meter)
- ri Inner Radius of Cylinder (Meter)
- ro Outer Radius of Cylinder (Meter)
- Rs Radius of Sphere (Meter)
- t Temperature Solid Cylinder (Kelvin)
- **T** Temperature (Kelvin)
- t₁ Temperature 1 (Kelvin)
- T₁ Surface Temperature (Kelvin)
- t₂ Temperature 2 (Kelvin)
- T_∞ Fluid Temperature (Kelvin)
- T_i Inner Surface Temperature (Kelvin)
- t_{max} Maximum Temperature of Plain Wall (Kelvin)
- T_{max} Maximum Temperature (Kelvin)
- To Outer Surface Temperature (Kelvin)
- T_w Surface Temperature of wall (Kelvin)
- X Thickness (Meter)
- X Location of Maximum Temperature (Meter)





Constants, Functions, Measurements used

- Function: In, In(Number)
 - The natural logarithm, also known as the logarithm to the base e, is the inverse function of the natural exponential function.
- Measurement: Length in Meter (m)
 Length Unit Conversion
- Measurement: Temperature in Kelvin (K)

 Temperature Unit Conversion
- Measurement: Thermal Conductivity in Watt per Meter per K (W/(m*K))

 Thermal Conductivity Unit Conversion
- Measurement: Heat Transfer Coefficient in Watt per Square Meter per Kelvin (W/m²*K)

 Heat Transfer Coefficient Unit Conversion
- Measurement: Power Density in Watt Per Cubic Meter (W/m³)

 Power Density Unit Conversion





Check other formula lists

- Conduction in Cylinder Formulas
- Conduction in Plane Wall Formulas
- Conduction in Sphere Formulas
- Conduction Shape Factors for Different Configurations Formulas
- Other shapes Formulas
- Steady State Heat Conduction with Heat Generation Formulas
- Transient Heat Conduction Formulas

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